Radiation Effect on MHD Fully Developed Mixed Convection in a Vertical Channel with Asymmetric Heating

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ABSTRACT

Effects of radiative heat transfer on an MHD fully developed mixed convective flow of a viscous incompressible electrically conducting fluid through a vertical channel with asymmetric heating of walls in the presence of a uniform transverse magnetic field has been studied. An exact solution of the governing equations has been obtained in closed form. It is observed that the velocity field is greatly influenced by the radiative heat transfer as well as buoyancy forces. The induced magnetic field decreases near the cool wall and it increases near the hot wall of the channel with an increase in radiation parameter. Further, an increase in radiation parameter leads to a decrease in the fluid temperature in the channel. A limiting consideration of the solutions of the governing equations of the flow are analyzed for $Ra \ll 1$.

Keywords: MHD mixed convective flow, Grashof number, radiation parameter, Prandtl number and asymmetric heating.

NOMENCLATURE

<table>
<thead>
<tr>
<th>Symbol</th>
<th>Description</th>
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<tr>
<td>$B_\text{x}$</td>
<td>induced magnetic field component along $x$-direction</td>
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<tr>
<td>$b_\text{x}$</td>
<td>non-dimensional induced magnetic field component</td>
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<td>$\tilde{B}$</td>
<td>the magnetic field vector</td>
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<td>$e_x$</td>
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<td>$g$</td>
<td>acceleration due to gravity</td>
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<td>$Gr_0, Gr_1$</td>
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<td>$M^2$</td>
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<td>$Pr$</td>
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<tr>
<td>$q_r$</td>
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<td>$Ra$</td>
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<td>$T_0$</td>
<td>temperature at entrance of channel</td>
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<td>$T_1$</td>
<td>temperature of hot wall</td>
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<td>$T_2$</td>
<td>temperature of cool wall</td>
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<td>$u$</td>
<td>velocity component in $x$-direction</td>
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<td>$u_1$</td>
<td>non-dimensional fluid velocity</td>
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<td>$(x, y)$</td>
<td>cartesian co-ordinates</td>
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<td>$\alpha$</td>
<td>non-dimensional pressure gradient</td>
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<tr>
<td>$\beta$</td>
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<td>$\mu_\text{r}$</td>
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<td>$\nu$</td>
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<td>$\lambda$</td>
<td>wave length</td>
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<tr>
<td>$\eta$</td>
<td>non-dimensional width of the channel</td>
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<tr>
<td>$\Theta$</td>
<td>dimensionless temperature</td>
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<tr>
<td>$\rho$</td>
<td>fluid density</td>
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<tr>
<td>$\tau_{c, r}$</td>
<td>shear stresses at cool and hot walls</td>
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</table>
1. INTRODUCTION

Heat transfer in free and forced convection in vertical channels occurs in any industrial processes and natural phenomena. Most of the interest in this subject results from its applications, for instance, in the design of cooling systems or electronic devices, chemical processing equipment, microelectronic cooling and in the field of solar energy collections. Since some fluids can also emit and absorb thermal radiation, it is of interest to study the effects of the magnetic field on the temperature distribution and heat transfer when the fluid is not only an electrical conductor but also when it is capable of emitting and absorbing radiation. Hence, heat transfer by thermal radiation is becoming of greater importance in space applications and higher operating temperatures. Ozisik (1989) has mentioned in an excellent review article that heat transfer by simultaneous radiation and convection has applications in numerous technological problems, including combustion, furnace design, the design of high-temperature gas-cooled nuclear reactors, nuclear-reactor safety, fluidized-bed heat exchangers, fire spreads, advanced energy conservation devices such as open-cycle coal and natural-gas-fired MHD, solar ponds, solar collectors, natural convection in cavities and many others. On the other hand, it is worth mentioning that heat transfer by simultaneous radiation and convection is very important in the context of space technology and processes involving high temperature. An excellent description of the fundamentals of thermal radiation has been presented in the book by Modest (2003).

For a comprehensive treatment of the radiation transfer and the interactions with convection the interested reader can consult also the books by Sprow and Hess (1970); Ozisik (1973); Siegel and Howell (1992). Aung (1972); Aung et al. (1972); Aung and Worku (1986); Barletta (2002); Boulama and Galanis (2004) deal with the evaluation of the temperature and velocity profiles for the vertical parallel-flow fully developed regime. As is well known, heat exchangers technology involves convective flows in vertical channels. In most cases, these flows imply conditions of uniform heating of a channel, which can be modelled either by uniform wall temperature or uniform heat flux thermal boundary conditions. Many process in new engineering areas occur at high temperatures and knowledge of radiative heat transfer becomes very important for the design of the pertinent equipment. Nuclear power plants, gas turbines and various propulsion devices for aircraft, missiles satellites and space vehicles are examples of such engineering areas. Cogley et al. (1968) have studied the differential approximation for radiative heat transfer in a non-grey gas near equilibrium. The hydrodynamic fully developed laminar convective flow through a vertical channel in the optically thin limit has been studied by Greif et al. (1971) whereas Gupta and Gupta (1974) have studied the same problem in the presence of a transverse magnetic field. The effects of radiative heat transfer on MHD flows in vertical channel have been studied a number of researches. Datta and Jana (1976) have discussed the effect of wall conductances on hydromagnetic convection of a radiating gas in a vertical channel. Ogulu and Motsa (2005) have studied the radiative heat transfer to magnetohydrodynamic Couette flow with variable wall temperature. Effect of radiation on unsteady free convection flow bounded by an oscillating plate with variable wall temperature have been described by Pathak et al. (2006). Sharma et al. (2007) have discussed the radiation effect on temperature distribution in three-dimensional Couette flow with suction / injection. The radiation effect on MHD free convection flow of a gas past a semi-infinite vertical plate have been studied by Takhar et al. (1996). The effects of wall conductance on MHD fully developed flow with asymmetric heating of the walls have been studied by Guria et al. (2007). Ghosh and Nandi (2000) have discussed magnetohydrodynamic fully developed combined convection flow between vertical plates heated asymmetrically, MHD fully developed mixed convection flow with asymmetric heating of the walls have been described by Ghosh et al. (2002). Pantokratoras (2006) has presented his results for a steady free convection flow between vertical parallel plates by considering different conditions on the wall temperature. The thermal radiation effect on fully developed mixed convection flow in a vertical channel have been examined by Grosan and Pop (2007). Suneetha et al. (2011) have presented the radiation and mass transfer effects on MHD free convective dissipative fluid in the presence of heat source/sink. Effects of thermal radiation on hydromagnetic flow due to a porous rotating disk with Hall effect have been studied by Anjali Devi and Uma Devi (2012). Baoku et al. (2012) have analyzed the influence of thermal radiation on a transient MHD Couette flow through a porous medium.

In the present paper, we study the effects of radiative heat transfer on MHD fully developed mixed convective flow in a vertical channel with the asymmetric heating of walls in the presence of a transverse magnetic field. We assume that the radiative heat flux follows a relation in an optically thin limit for a non-gray gas near equilibrium. The closed form solutions for velocity, temperature, shear stresses, rate of heat transfer and critical Grashof number are presented. Flow and heat transfer results for a range of values of the pertinent parameters have been reported. It is observed that the velocity field is greatly influenced by the radiative heat transfer as well as buoyancy forces. The induced magnetic field decreases near the cool wall and it increases near the hot wall of the vertical channel with an increase in radiation parameter. Further, an increase in radiation parameter leads to decrease the fluid temperature in the channel.

2. FORMULATION OF THE PROBLEM AND ITS SOLUTION

Consider a steady MHD fully developed mixed convective flow of a viscous incompressible electrically conducting fluid confined between
vertical walls. The channel walls are at a distance $d$ apart. Choose a Cartesian co-ordinates system with $x$ -axis in the upward direction along the cool wall in the direction of flow and the axis of $y$ is perpendicular to it. The wall at $y = 0$ has a uniform temperature $T_i$ while the wall at $y = d$ is subjected to a uniform temperature $T_e$, where $T_e > T_i$. A uniform magnetic field of strength $B_0$ is imposed perpendicular to the channel walls. The flow is due to buoyancy force, difference in temperature and in the presence of pressure gradient. Since the channel walls are infinitely long along the $x$-direction, all physical quantities, are functions of $y$ only. The velocity components are $(u,v)$ relative to the Cartesian frame of reference.

\[
0 = k \frac{d^2 T}{dy^2} - \frac{\partial q}{\partial y}, \quad (4)
\]

where $\nu$ is the kinematic viscosity, $\mu$, the magnetic permeability, $\sigma$ the conductivity of the fluid, $g$ the acceleration due to gravity, $k$ the thermal conductivity and $q$, the radiative heat flux.

It has been shown by Cogley et al. (1968) that in the optically thin limit for a non-gray gas near equilibrium, the following relation holds

\[
\frac{\partial q}{\partial y} = 4(T - T_i) \int_0^K \frac{\partial (e_{'0})}{\partial (T')} d\lambda, \quad (5)
\]

where $K_{h0}$ is the absorption coefficient, $\lambda$ is the wave length, $e_{'0}$ is the Planck's function and subscript $'0'$ indicates that all quantities have been evaluated at the temperature $T_0$ which is the temperature at entrance of the channel.

On the use of (5), the Eq.(4) becomes

\[
0 = k \frac{d^2 T}{dy^2} - 4T(T - T_i), \quad (6)
\]

where

\[
I = \int_0^K \frac{\partial (e_{'0})}{\partial (T')} d\lambda
\]

In asymmetric heating of the walls, the velocity, magnetic and temperature boundary conditions are respectively,

\[
u = 0, \quad T = T_e \quad \text{and} \quad B = 0 \quad \text{at} \quad y = 0,
\]

\[
u = 0, \quad T = T_i \quad \text{and} \quad B = 0 \quad \text{at} \quad y = d, \quad (7)
\]

assuming the walls are electrically non-conducting.

Introducing the non-dimensional variables

\[
e = \frac{y}{d}, \quad u = \frac{ud}{\nu}, \quad b = \frac{B_0}{\mu \nu}, \quad T = \frac{T - T_i}{T_e - T_0}, \quad \theta = \frac{T - T_0}{T_e - T_0}, \quad (8)
\]

Eqs. (2), (3) and (6) become

\[
d^2 u + M: d db + Gr \theta + \alpha = 0, \quad (9)
\]

\[
d^2 b + d u = 0, \quad (10)
\]

\[
d^2 \theta + Ra \theta = 0, \quad (11)
\]

where $M = B_0 \mu d \left(\frac{\sigma}{\rho_0 \nu^2}\right)^{\frac{1}{2}}$ is the Hartmann number, $Gr = \frac{g \beta(T_e - T_i) d^3}{\nu^2}$ the Grashof number and $Ra = \frac{4d^2}{k}$ the radiation parameter and

\[
\alpha = \frac{d^2}{\nu^2} \left(-\frac{\partial p}{\partial x}\right) \quad \text{the non-dimensional pressure gradient.}
\]

The boundary conditions given by (7) become

\[
u_i = 0, \quad \theta = \eta \quad \text{and} \quad b_i = 0 \quad \text{at} \quad \eta = 0
\]

\[
u_i = 0, \quad \theta = 1 \quad \text{and} \quad b_i = 0 \quad \text{at} \quad \eta = 1, \quad (12)
\]

where $\eta_i = \frac{T_i - T_0}{T_1 - T_0}$ is the temperature difference ratio.

Solution of Eqs. (9) to (11) subject to the boundary
conditions (12) are

\[
\theta(\eta) = \frac{\sinh(\sqrt{Ra} \eta) + \sinh(\sqrt{Ra}(1 - \eta))}{\sinh(\sqrt{Ra})}, \quad Ra \neq M^2
\]

\[
\sinh(M \eta) + \eta \sinh(M(1 - \eta)) = \frac{\sinh(\sqrt{Ra} \eta) + \sinh(\sqrt{Ra}(1 - \eta))}{\sinh(\sqrt{Ra})}, \quad Ra = M^2.
\]

\[
\eta(\eta) = \left\{ \begin{array}{l}
\frac{\alpha}{M^2} + c \left[1 - \frac{\sinh(M \eta)}{\sinh(M)}\right]
+ Gr \left[\frac{\sinh(M \eta)}{\sinh(M)}\right], \\
\frac{\alpha}{M^2} + c \left[1 - \frac{\sinh(M \eta)}{\sinh(M)}\right]
+ Gr \left[\frac{\sinh(M \eta)}{\sinh(M)}\right], \\
\end{array} \right. \quad Ra = M^2;
\]

where

\[
\alpha = \frac{Gr(1 + \tau_r) + 1 + \cosh(M \eta)}{M \sinh(M) + \cosh(M \eta)}, \quad Ra = M^2.
\]

The parameter \(\alpha\) is given by (14). In the case of without wall conductance.

3. EXPRESSION FOR PRESSURE GRADIENT

It is noticed from the Eqs. (14) and (15) that the parameter \(\alpha\) is still to be evaluated. Using the rate of mass flow

\[
\int u \, d\eta = 1,
\]

we have, on the substitution of the value of \(\eta\), which is obtained from Eq. (14) as

\[
\alpha = \left\{ \begin{array}{l}
\frac{2M^2}{M \sinh(M) + 2(1 - \cosh(M))}, \\
\frac{2M^2}{M \sinh(M) + 2(1 - \cosh(M))}, \quad Ra = M^2;
\end{array} \right.
\]

4. RESULTS AND DISCUSSION

To study the effects of radiative heat transfer and the magnetic field on the MHD fully developed flow with asymmetric heating of the walls, the dimensionless velocity \(u_1\), the induced magnetic filed \(b_1\), and temperature distribution \(\theta\) are depicted graphically against \(\eta\) for several values of radiation parameter \(Ra\), magnetic parameter \(M^2\), bounanity parameter \(Gr\) and temperature difference ratio \(\tau_r\) in Figs.2 to 13. Figures 2 and 3 depicts the effects of the radiative heat transfer and magnetic field on the velocity field. It is seen from Fig.2 that the fluid velocity \(u_1\) increases in the range \(0 \leq \eta \leq 0.38\) while it decreases in the range \(0.38 < \eta \leq 0.86\) and again it increases in the range \(0.86 < \eta \leq 1\) with an increase in radiation parameter \(Ra\). It is manifested that there is a closeness of the curves near the hot wall. Fig.3 reveals that the fluid velocity \(u_1\) increases in the range \(0 \leq \eta \leq 0.42\) while it decreases in the range \(0.42 < \eta \leq 1\) with an increase in magnetic parameter \(M^2\). It means that the Lorentz force imposed by a transverse magnetic field to an electrically conducting fluid, which slows down the fluid motion near the hot wall and enhances the fluid motion near cool wall. It is also manifested that there is a closeness of the curves near the hot wall. It is noticed from Fig.4 that the fluid velocity \(u_1\) decreases in the region \(0 \leq \eta \leq 0.53\) and it increases in the region \(0.53 < \eta \leq 1\) with increase in Grashof number \(Gr\). Fig.5 shows that with an increase in \(\tau_r\), the fluid velocity \(u_1\) increases in the region \(0 \leq \eta \leq 0.53\) and it decreases in the region \(0.53 \leq \eta \leq 1\). It is
observed from Fig.6 that the induced magnetic field $b_i$ decreases at any point near the cool wall and it increases near the hot wall with an increase in $Ra$. Fig.7 shows that the induced magnetic field $b_i$ decreases with an increase in $M^2$. It is seen from Fig.8 that the induced magnetic field $b_i$ increases with an increase in $Gr$. Fig.9 reveals that the induced magnetic field $b_i$ decreases with an increase in $r_t$. The temperature profiles have been drawn for different values of $Ra$ and $r_t$ in Figs.10 and 11. It is seen from Figs.10 and 11 that the fluid temperature $\theta$ decreases with an increase in radiation parameter $Ra$ while it increases with an increase in temperature difference ratio parameter $r_t$.

Fig. 2. Variation of velocity for different $Ra$ when $M^2 = 5$, $r_t = 0.4$ and $Gr = 100$

Fig. 3. Variation of velocity for different $M^2$ when $Ra = 4$, $r_t = 0.4$ and $Gr = 100$

Fig. 4. Variation of velocity for different $Gr$ when $M^2 = 5$, $Ra = 4$ and $r_t = 0.4$

Fig. 5. Variation of velocity for different $r_t$ when $M^2 = 5$, $Ra = 4$ and $Gr = 100$

Fig. 6. Variation of induced magnetic field for different $Ra$ when $M^2 = 5$, $r_t = 0.4$ and $Gr = 100$
One of the important characteristics of this problem is the shear stress at the walls. The non-dimensional shear stress at the cool wall ($\eta = 0$) and hot wall ($\eta = 1$) are respectively given by

$$\tau_{0} = \left( \frac{du}{d\eta} \right)_{\eta=0} \quad \text{and} \quad \tau_{1} = \left( \frac{du}{d\eta} \right)_{\eta=1}, \quad (20)$$

where

$$\frac{M'(cosh M - 1)}{M sinh M + 2(1-cosh M)} \left[ 1 + Gr(1 + \eta) \left( 1 - \frac{1-cosh\sqrt{Ra}}{M sinh M} \right) \right] \frac{Gr}{Ra - M^2} + \frac{Gr}{Ra - M^2} \left[ \frac{M(1 - \tau_{0}cosh M)}{sinh M} \cdot \frac{\sqrt{Gr}(1 - \tau_{0}cosh M)}{sinh\sqrt{Ra}} \right], \quad Ra = M^2 +$$

$$\left( \frac{du}{d\eta} \right)_{\eta=0} =$$

$$\frac{M'(cosh M - 1)}{M sinh M + 2(1-cosh M)} \left[ 1 + Gr(1 + \eta) \left( 1 - \frac{1-cosh\sqrt{Ra}}{M sinh M} \right) \right] \frac{Gr}{Ra - M^2} + \frac{Gr}{Ra - M^2} \left[ \frac{M(1 - \tau_{0}cosh M)}{sinh M} \cdot \frac{\sqrt{Gr}(1 - \tau_{0}cosh M)}{sinh\sqrt{Ra}} \right], \quad Ra = M^2 +$$

and

$$\tau_{0} = \left( \frac{du}{d\eta} \right)_{\eta=0} \quad \text{and} \quad \tau_{1} = \left( \frac{du}{d\eta} \right)_{\eta=1}, \quad (20)$$
The values of non-dimensional shear stresses at the walls $\eta = 0$ and $\eta = 1$ are shown graphically against $r_c$ for different values of $Ra$ and $M^2$ in Figs.12 and 13. It is observed from Fig.12 that for fixed values of $M^2$ and $Gr$ the shear stress $\tau_{\eta}$ at the cool wall increases while the shear stress $\tau_{1\eta}$ at the hot wall decreases with an increase in radiation parameter $Ra$. On the other hand, Fig.13 shows that the shear stress $\tau_{r_c}$ at the cool wall increases while the shear stress $\tau_{r_c}$ at the right wall decreases with increase in $M^2$. It is interesting to note that the shear stress due to the flow does not vanish at the walls $\eta = 0$ and $\eta = 1$ when buoyancy forces $Gr = 0$. Thus we arrive an interesting conclusion that there is no flow reversal in the absence of the buoyancy forces.

The shear stresses at the cool and hot wall vanish if

$$
G_{\eta_0} = \begin{cases}
\frac{(Ra - M^2)M^2(1 - \cosh M)}{(A + B)[M \sinh M + 2(1 - \cosh M)]}, & Ra \neq M^2 \\
2M^2(1 - \cosh M), & Ra = M^2,
\end{cases}
$$

(23)

| $Gr_0 \times 10^{-5}$ at the cool wall. $Gr_0$ |
|-----------------|-------|-------|-------|-------|-------|-------|
| $M^2$ | 2 | 4 | 6 | 0 | 0.2 | 0.4 |
| 5 | 0.1821947 | 0.2327067 | 0.2946396 | 0.1056287 | 0.1453024 | 0.2327067 |
| 10 | 0.2102455 | 0.2710896 | 0.347127 | 0.1214226 | 0.1677217 | 0.2710896 |
| 15 | 0.2385835 | 0.3102064 | 0.4012581 | 0.1373196 | 0.1903684 | 0.3102064 |
| 20 | 0.2671151 | 0.3498836 | 0.4567396 | 0.1532741 | 0.2131661 | 0.3498836 |

Fig. 12. Shear stress for different $Ra$ when $M^2 = 5$, $Ra = 4$ and $Gr = 50$

Fig. 13. Shear stress for different $M^2$ when $M^2 = 5$, $r_c = 0.4$ and $Gr = 50$
The values of the critical Grashof numbers $Gr_e$ and $Gr_t$, due to the flow at the cool wall $\eta = 0$ and hot wall $\eta = 1$ are entered in the Tables 1 and 2 for different values of magnetic parameter $M^2$, radiation parameter $Ra$ and the temperature difference ratio parameter $r_t$. It is seen from the Table 1 that the critical Grashof number $Gr_e$ at the cool wall ($\eta = 0$) due to the flow increases with increase in either $Ra$ or $r_t$ or $M^2$. Table 2 shows that the critical Grashof number $Gr_t$ at the hot wall ($\eta = 1$) due to the flow increases with an increase in either $M^2$ or $r_t$. On the other hand, with increase in the radiation parameter $Ra$ , the critical Grashof number $Gr_t$ decreases.

In the absence of radiative heat transfer ($Ra = 0$), the critical Grashof numbers $Gr_e$ and $Gr_t$ are given by

$$Gr_e = \frac{2M^2(\cosh M - 1)}{(1 - r_t)(M^2(1 + \cosh M) + 4\cosh M - 4M(1 + \cosh M))},$$  
(25)

$$Gr_t = -Gr_e,$$  
(26)

which are identical with the Eq. (39) of Guria et al. (2007).

### 4.1. Limiting Case

Now, we discuss the case when the radiation parameter is $Ra \ll 1$. In this case, Eqs. (13) to (15) become

$$\theta(\eta) = \eta + \frac{Ra}{6}(\eta - 1) + r_t\left[1 - \eta - \frac{Ra}{6}(1 - \eta)(\eta - 2)\right],$$  
(27)

$$u_r(\eta) = \frac{\alpha}{M^2} + c\left[1 - \frac{\sinh M - \eta}{\sinh M(1 - \eta)}\right] + \frac{Gr}{Ra - M^2}\left[\frac{\sinh M + r_t}{\sinh M} - \frac{\sinh M(1 - \eta)}{\sinh M}\right],$$  
(28)

$$b_r(\eta) = \frac{\alpha}{2M^2} + \frac{Gr(1 - r_t)}{2(Ra - M^2)}\left[1 + \frac{\cosh M}{M\sinh M + c\eta} - \frac{\alpha}{M^2} + c\left[\frac{\cosh M\eta - \cosh M(1 - \eta)}{\cosh M + \cosh M}\right] - \frac{\alpha}{M^2} + c\left[\frac{\cosh M\eta + \cosh M(1 - \eta)}{\cosh M + \cosh M}\right]\right. - \frac{Gr}{Ra - M^2}\left[\frac{\cosh M\eta}{M\sinh M} + r_t\frac{\cosh M(1 - \eta)}{M\sinh M}\right] - \frac{3Gr}{(Ra - M^2)(Ra + 6)}\frac{1}{2}

$$

where

$$c = \frac{-\alpha}{M^2} + \frac{Gr(1 + r_t)}{2(Ra - M^2)}\left[\frac{M\sinh M + 2(1 - \cosh M)}{2\cosh M - 1}\right],$$

$$\alpha = \frac{2M^2(\cosh M - 1)}{M\sinh M + 2(1 - \cosh M)}\frac{Gr(1 + r_t)}{2(Ra - M^2)}.$$  
(30)

In limit $Ra \to 0$, Eqs. (27) to (28) for the temperature, the velocity and the induced magnetic field yield respectively

$$\theta(\eta) = \eta + r_t(1 - \eta),$$

(31)

$$u_r(\eta) = \frac{1}{M^2}\left[Gr(1 + r_t)\left[\eta - \frac{\sinh M}{\sinh M}\right]\right] + Gr(1 - r_t)\left[\frac{1}{2}\eta^2 - \frac{\cosh M\eta}{M\sinh M}\right] + c\eta + c_r,$$  
(32)

$$b_r(\eta) = \frac{1}{2M^2}\left[Gr(1 + r_t)\left[\eta - \frac{\sinh M}{\sinh M}\right]\right] + Gr(1 - r_t)\left[\frac{1}{2}\eta^2 - \frac{\cosh M\eta}{M\sinh M}\right] + c\eta + c_r,$$  
(33)

where

$$c = \frac{r_t}{M^2} + \frac{1}{2}Gr(1 - r_t)\left[\frac{M\sinh M + 2(1 - \cosh M)}{2\cosh M - 1}\right],$$

$$c_r = \frac{1}{2M^2}\left[Gr(1 + r_t) + \frac{1}{2}Gr(1 - r_t)\left[\frac{M\sinh M - 2(1 - \cosh M)}{M\sinh M}\right]\right].$$

(34)

The velocity and the induced magnetic field given by (32) and (33) coincide with Eqs. (14) and (15) of Guria et al. (2007) in the case of without wall conductance.

### 5. CONCLUSION

An MHD fully developed mixed convection in a vertical channel in the presence of radiation have been studied. It is seen that the fluid velocity is strongly affected by the radiative heat transfer as well as buoyancy force. The induced magnetic field decreases near the cool wall and it increases near the hot wall of the channel with an increase in radiation parameter. Radiation decreases the fluid temperature. It is interesting to note that the shear stress due to the flow does not vanish at the channel walls when $Gr = 0$ and hence there is no flow reversal in the absence of the buoyancy force. This model finds applications in the design of cooling systems, chemical processing equipments and the field of solar energy collections.

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**APPENDIX**

\[
A = \begin{cases}
M^2(1 + r_j)(1 - \cosh M - 1) \frac{M - \cosh M}{M \sinh M + 2(1 - \cosh M)} \sinh \frac{M - \cosh M}{\sqrt{Ra} \sinh \sqrt{Ra}}, & \text{Ra} \neq M^2 \\
1 - \cosh M \frac{M - \cosh M}{M \sinh M + 2(1 - \cosh M)} \sqrt{Ra} \sinh \sqrt{Ra}, & \text{Ra} = M^2 \\
1 - \cosh M \frac{M - \cosh M}{M \sinh M + 2(1 - \cosh M)} \sqrt{Ra} \sinh \sqrt{Ra}, & \text{Ra} \neq M^2 \\
1 - \cosh M \frac{M - \cosh M}{M \sinh M + 2(1 - \cosh M)} \sqrt{Ra} \sinh \sqrt{Ra}, & \text{Ra} = M^2
\end{cases}
\]

\[
B = \begin{cases}
\frac{M(1 - r_j \cosh M)}{\sinh M} \frac{\sqrt{Ra}(1 - r_j \cosh \sqrt{Ra})}{\sqrt{Ra}}, & \text{Ra} \neq M^2 \\
\frac{M(1 - r_j \cosh M)}{\sinh M} \frac{\sqrt{Ra}(1 - r_j \cosh \sqrt{Ra})}{\sqrt{Ra}}, & \text{Ra} = M^2 \\
\frac{M(1 - r_j \cosh M)}{\sinh M} \frac{\sqrt{Ra}(1 - r_j \cosh \sqrt{Ra})}{\sqrt{Ra}}, & \text{Ra} \neq M^2 \\
\frac{M(1 - r_j \cosh M)}{\sinh M} \frac{\sqrt{Ra}(1 - r_j \cosh \sqrt{Ra})}{\sqrt{Ra}}, & \text{Ra} = M^2
\end{cases}
\]