

## Mixed Convection Magnetic Nanofluid Flow past a Rotating Vertical Porous Cone

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### ABSTRACT

Magnetic nanofluids (MNFs) have been the focus of extensive research nowadays owing to their potential usefulness as a transfer medium. This study is concerned with the boundary layer flow and heat transfer of MNF past a rotating vertical cone with the embedment of the porosity regime and mixed convection. The buoyancy opposing flow on the combined free and forced convection is being emphasized in this study to evaluate the behavior of the fluid within this region and predict the point of the boundary layer transition. The initial formulation of the model is simplified appropriately by employing the suitable similarity transformation. The package of `bvp4c` MATLAB is employed to execute the numerical solutions. Analysis of stability is also reported. Due to the mixed convection parameter, the opposing flow contributes towards two different alternative solutions, but the second solution is not stable. A higher local Nusselt number are achieved by increasing the concentration of magnetic nanofluid up to 2% and enlarging the mixed convection parameter under the influence of the porosity regime in the vertical rotating cone. It has been established in this study that the addition of cobalt ferrite as the magnetic nanoparticles (MNPs) is proven to have the ability in enhancing the thermal performance of the fluid.

**Keywords:** Mixed convection; Nanofluid; Porous medium; Cone; Stability analysis.

### NOMENCLATURE

|                    |                                      |                |                                   |
|--------------------|--------------------------------------|----------------|-----------------------------------|
| $C_{f,x}, C_{f,y}$ | skin friction in $x, y$ -directions  | $\varepsilon$  | porosity parameter                |
| $Da^{-1}$          | inverse Darcy number                 | $\beta_f$      | thermal expansion of base fluid   |
| $f_c$              | friction factor                      | $\beta_{nf}$   | thermal expansion of nanofluid    |
| $Gr_L$             | Grashof number                       | $\beta_s$      | thermal expansion of nanoparticle |
| $K$                | permeability parameter               | $\gamma$       | eigenvalue parameter              |
| $k_f$              | thermal conductivity of base fluid   | $\lambda$      | mixed convection parameter        |
| $k_{nf}$           | thermal conductivity of nanofluid    | $\mu_f$        | dynamic viscosity of base fluid   |
| $k_s$              | thermal conductivity of nanoparticle | $\mu_{nf}$     | dynamic viscosity of nanofluid    |
| $L$                | characteristic length of cone        | $\rho_f$       | density of base fluid             |
| $Nu_x$             | local Nusselt number                 | $\rho_{nf}$    | density of nanofluid              |
| Pr                 | Prandtl number                       | $\rho_s$       | density of nanoparticle           |
| $r$                | cone radius                          | $(\rho C_p)_f$ | heat capacity of base fluid       |
| $Re_L$             | Reynolds number                      |                |                                   |

|            |                                   |                   |                               |
|------------|-----------------------------------|-------------------|-------------------------------|
| $T_w$      | cone surface temperature          | $(\rho C_p)_{nf}$ | heat capacity of nanofluid    |
| $T_\infty$ | free stream temperature           | $(\rho C_p)_s$    | heat capacity of nanoparticle |
| $T_0$      | characteristic temperature        | $\tau$            | dimensionless time variable   |
| $t$        | time                              | $\phi$            | nanoparticle volume fraction  |
| $u, v, w$  | velocity in $x, y, z$ -directions | $\Omega$          | angular velocity              |

## 1. INTRODUCTION

The urgent demand for heat exchangers and coolants with enhanced performance has led to the innovation of nanofluid. This fluid consists of the colloidal diffusion of solid particles of nano-sized that are suspended in a carrier fluid. The original idea of solid particle dispersion was first developed by Maxwell (1873) to augment the thermal properties. However, because of the size of the solid particles, mostly in micro-sized; clogging and sedimentation in the flow passage have become a challenge due to the agglomeration among the solid particles (Ali *et al.*, 2018). For that reason, Choi and Eastman (1995) came up with the idea of utilizing smaller size solid particles, which are nanoparticles, to overcome this issue. Several reviews in myriad aspects of nanofluid are available in this literature for further reading: (see Saidur *et al.*, 2011; Yu and Xie, 2012; Akilu *et al.*, 2016; Devendiran and Amirtham, 2016; Prasad *et al.*, 2017; Ahmadi *et al.*, 2018).

Magnetic nanofluid (MNF), also known as a ferrofluid, is one of the reliable emerging types of nanofluid that receive great interest among researchers due to its special magnetic features. MNF is made up of the stable colloidal mixtures of superparamagnetic nanoparticles such as iron and cobalt (ferromagnetic material), as well as magnetite (ferromagnetic material) that is dispersed in a non-magnetic carrier fluid viz. oil, water, or ethylene glycol (Genc & Derin, 2014; Nkurikiyimfura *et al.*, 2013). Historically, this fluid was initially suggested by Steve Papell (at NASA) to make a suitable liquid rocket fuel suspended with finely-ground iron oxide (Stephen, 1965). Since then, this fluid has been used to solve many complex activities, including in biomedical (e.g., drug delivery, contrast agent/tracer, magnetic resonance image technology (MRI)), thermal engineering (e.g., thermal conductivity, heat transfer enhancement), and machine/device design (e.g., inertia damper, magnetic sealing, lubrication, film bearing, loudspeaker) applications (Marszałł, 2011; Khairul *et al.*, 2017; Kumar & Subudhi, 2018; Kole & Khandekar, 2021).

Multidisciplinary strategies are required to understand the properties of MNF. One of them is by studying its flow dynamic and heat transfer properties at the boundary layer so that the flow can be modelled and controlled accordingly when applied to a specific application. Qasim *et al.* (2014) examined the heat transmission performance at the boundary layer of magnetite-water MNF along an expanding cylinder. The local Nusselt number for this fluid increases and aligns with the non-magnetic (alumina-water) nanofluid only if the extra magnetic field is applied. Though the non-magnetic

nanoparticle has a higher thermal conductivity than the magnetic nanoparticle, the performance of MNF can be manipulated with the external magnetic field. Another comparison study between MNF dan non-MNF was also conducted by Gul *et al.* (2015) with the inclusion of an external magnetic field and mixed convection along a vertical channel. The temperature distribution of MNF is observed to be lower than non-MNF, but the temperature distribution can be improved by magnifying the magnetic nanoparticles concentration. Their findings align with the prior experimental studies examined by Colla *et al.* (2012). Later, Raju and Sandeep (2017) evaluate the unsteady MNF with water-based cobalt ferrite nanoparticles by using Casson model. They concluded that the spike in the concentration of the nanoparticles and buoyancy had initiated the skin friction to get larger.

Jusoh *et al.* (2018) employed three different base liquids towards the magnetite MNF in their study on the rotating flow past the exponentially expanding/contracting sheet. The MNF with kerosene as the base liquid is calculated to have the highest heat transfer efficiency compared to water and methanol. Besides, Sulochana *et al.* (2018) also considered magnetite-water and magnetite-methanol as the MNF to be investigated in the moving horizontal needle. Ahmed *et al.* (2019) researched the radiative MNF flow over a wedge for several base liquids and nanoparticles. The stagnation point flow with Newtonian heating of magnetite nanofluid was disclosed by Mohamed *et al.* (2019). Magnetite, cobalt ferrite, and manganese-zinc ferrite nanoparticles are adopted by Bognár and Hriczó (2020) to explore the boundary layer flow of MNF past an expanding flat sheet. Khan *et al.* (2020) revealed the characteristic of micropolar MNF of second-order velocity slip flow through a two-phase model due to a stretchable surface. Rasli and Ramli (2021) addressed the study on MNF with three different magnetic nanoparticles over the exponentially stretchable/shrinkable sheet with magnetohydrodynamic. Recently, Anuar *et al.* (2021) contemplated the flow of hybrid MNF with heat source/sink due to the stagnation point on a stretchable and shrinkable sheet. The viscous dissipation effect has been used by Hamid *et al.* (2022) to explore the flow phenomena of dusty MNF on the non-isothermal movable surface. Several other latest pertinent studies on MNF are extractable through this list: (Bhandari, 2021; Jalili *et al.*, 2021; Mohamed *et al.*, 2021; Nayak *et al.*, 2021; Saranya *et al.*, 2021; Uddin *et al.*, 2021).

Furthermore, instead of suspending stronger thermal conductivity nanoparticles towards the base fluid, changing the flow geometry is also one of the

techniques that could be utilized to improve the heat transfer performance. Karuppasamy *et al.* (2020) concluded that the cone shape inserts in the heat exchanger tube significantly improve the heat transfer process. Historically, the work on vertical cone was pioneered by Kumari *et al.* (1989) to elucidate the flow and heat transfer for mixed convection. Since then, the utilization of cone geometry has been considered by many researchers to investigate its effectiveness either by using the numerical or experimental approach. The modified rotating reactor with a cone shape has been developed by Guoxin *et al.* (2008) for the thermochemical treatment of coal with a solid heat carrier. The conical shape coil with different cone angles was also used by Purandare *et al.* (2015) to analyze the thermal capability of the heat exchanger. Palanisamy & Mukesh Kumar (2019) experimented the heat transfer in the heat exchanger that made up of cone helically coiled tube with the inclusion of nanofluid. The exploration on nanofluid flooding effect for the recovery oil process enhancement by using the incomplete porous cone was experimented by Hemmat Esfe *et al.* (2020). This kind of geometry has captivated the interest of many researchers since it is practically important in real applications. To name a few, it is utilized in space technology, automotive, nuclear safety management, biomedical, aerospace, heat exchanger, oil recovery, and radiology (Raju *et al.*, 2017).

The investigations as mentioned previously are diversified accordingly with different kind of effects and geometries to simulate the behavior of MNF in actual boundary layer phenomena. Furthermore, so far, we have witnessed that the numerical investigation on mixed convection magnetic nanofluid (MNF) flow past a rotating vertical porous cone has not yet been addressed. Hence, we believed that this study could fill the research gap significantly with its originality for future insight. The highlights of the addressed study are listed as follows:

- We consider the inclusion of cobalt ferrite-water (CoFe<sub>2</sub>O<sub>4</sub>-H<sub>2</sub>O) MNF to extend the previous study by Mallikarjuna *et al.* (2016) as their study is only limited to a regular viscous fluid.
- The Tiwari and Das model for nanofluid is considered in this study instead of Buongiorno model.
- The mixed convection with opposing flow is considered, while the study by Mallikarjuna *et al.* (2016) only emphasized the assisting flow.
- The trusted solver (bvp4c MATLAB) is implemented to solve the flow problem, and the results are validated with several existing studies.
- Dual solutions are presented together with the critical point of the boundary layer separation.
- The study is completed with stability analysis in providing the conclusion about the stability feature of the generated dual solutions.
- The increment of CoFe<sub>2</sub>O<sub>4</sub> volume fraction up to 2% is numerically verified to enhance the local Nusselt number.

## 2. MATHEMATICAL MODEL

As visualized in Fig. 1, the mixed convection MNF flow past a vertical rotating cone in a porous medium with an angular velocity  $\Omega$  is considered, where  $x$  - axis is along a meridional section,  $y$  -axis is along a circular section, and the  $z$  -axis is normal to the cone surface. Other assumptions that we intend to make are:

- The flow is steady and laminar being at  $z \geq 0$ .
- Cobalt ferrite and water are chosen as the magnetic nanoparticles (MNPs) and the base liquid, respectively, to form MNF.
- The cone surface is preserved at a temperature  $T_w(x) = T_\infty + T_0(x/L)$ , where  $T_0$  is a characteristic temperature of the fluid, with  $T_0 > 0$  for the assisting flow,  $T_0 < 0$  for the opposing flow and  $T_0 = 0$  for the forced convection flow, and  $T_\infty$  is the free-stream temperature, while  $L$  is the characteristic length of the cone.
- The porous medium is in the local thermal equilibrium.

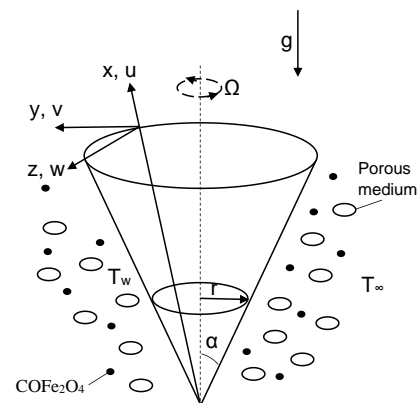


Fig. 1. Model illustration with coordinate system.

Keeping these assumptions in mind, and with the reference from Mallikarjuna *et al.* (2016) and Ahmed *et al.* (2019), the mathematical model are formulated as

$$\frac{\partial u}{\partial x} + \frac{\partial w}{\partial z} + \frac{u}{x} = 0 \tag{1}$$

$$\varepsilon^{-2} \left( u \frac{\partial u}{\partial x} + w \frac{\partial u}{\partial z} - \frac{v^2}{x} \right) = \varepsilon^{-1} \frac{\mu_{nf}}{\rho_{nf}} \frac{\partial^2 u}{\partial z^2} - \frac{\mu_{nf}}{\rho_{nf}} \frac{u}{K} + \frac{(\rho\beta)_{nf}}{\rho_{nf}} (T - T_\infty) g \cos \alpha \tag{2}$$

$$\varepsilon^{-2} \left( u \frac{\partial v}{\partial x} + w \frac{\partial v}{\partial z} + \frac{uv}{x} \right) = \varepsilon^{-1} \frac{\mu_{nf}}{\rho_{nf}} \frac{\partial^2 v}{\partial z^2} - \frac{\mu_{nf}}{\rho_{nf}} \frac{v}{K} \tag{3}$$

$$u \frac{\partial T}{\partial x} + w \frac{\partial T}{\partial z} = \frac{k_{nf}}{(\rho C_p)_{nf}} \frac{\partial^2 T}{\partial z^2} \quad (4)$$

subject to

$$\left. \begin{aligned} v = \Omega r, u = 0, w = 0, \\ T = T_w(x) = T_\infty + T_0 \left( \frac{x}{L} \right) \end{aligned} \right\} \text{ at } z = 0 \quad (5)$$

$$u \rightarrow 0, v \rightarrow 0, T \rightarrow T_\infty \text{ as } z \rightarrow \infty$$

where  $u, v$  and  $w$  are the velocity components along  $x, y, z$  directions,  $r = x \sin \alpha$  is the radius of the cone at the base ( $x = L$ ),  $\varepsilon$  is the porosity parameter and  $K$  is the porous medium permeability.

It should be noted that the MNF in this study considers the thermophysical properties such as, density  $\rho_{nf}$ , heat capacity  $(\rho C_p)_{nf}$ , dynamic viscosity  $\mu_{nf}$ , thermal conductivity  $k_{nf}$ , and thermal expansion  $\beta_{nf}$  which the correlations are given in Table 1 (Takabi & Salehi, 2015). The subscript of  $f$  and  $s$  refer to the base liquid and MNP, separately. The thermal and physical characteristics for base liquid and MNP are given in Table 2 (Ahmed *et al.*, 2019; Raju & Sandeep, 2017; Gul *et al.*, 2015), where  $\phi$  is the MNP volume fraction and  $Pr = v_f (\rho C_p)_f / k_f$  is Prandtl number.

**Table 1 Correlation of thermophysical properties of MNF**

| Properties           | Correlations  |
|----------------------|---|
| Density              | $\rho_{nf} = (1 - \phi) \rho_f + \phi \rho_s$   |
| capacity Heat        | $(\rho C_p)_{nf} = (1 - \phi) (\rho C_p)_f + \phi (\rho C_p)_s$                           |
| Dynamic viscosity    | $\frac{\mu_{nf}}{\mu_f} = \frac{1}{(1 - \phi)^{2.5}}$                                     |
| Thermal conductivity | $\frac{k_{nf}}{k_f} = \frac{k_s + 2k_f - 2\phi(k_f - k_s)}{k_s + 2k_f + \phi(k_f - k_s)}$ |
| Thermal expansion    | $\beta_{nf} = \frac{1}{\rho_{nf}} (\phi \rho_s \beta_s + (1 - \phi) \rho_f \beta_f)$      |

**Table 2 Thermal and physical characteristics for MNF compositions**

| Properties                  | Water (H <sub>2</sub> O) | Cobalt ferrite (CoFe <sub>2</sub> O <sub>4</sub> ) |
|-----------------------------|--------------------------|--|
| $\rho$ (kg/m <sup>3</sup> ) | 997.1                    | 4907   |
| $C_p$ (J/kgK)               | 4179                     | 700  |
| $k$ (W/mk)                  | 0.613                    | 3.7  |
| $\beta$ (1/K)               | $21 \times 10^{-5}$      | $2.1 \times 10^{-5}$                               |
| Pr                          | 6.96                     | -  |
| $\phi$                      | -                        | 1%-2%  |

The boundary conditions Eq. (5) suggest the following similarity variables (Mallikarjuna *et al.*, 2016)

$$\left. \begin{aligned} u = x \Omega \sin \alpha f(\eta), v = x \Omega \sin \alpha g(\eta), \\ w = \sqrt{v_f \Omega \sin \alpha} h(\eta), \\ \theta(\eta) = \frac{T - T_\infty}{T_w - T_\infty}, \eta = z \sqrt{\Omega \sin \alpha / v_f} \end{aligned} \right\} \quad (6)$$

where prime denotes the differentiation of the function concerning  $\eta$ .

Applying the transformation into Eqs. (1) to (5), we get the new transformed equations

$$f = -\frac{1}{2} h' \quad (7)$$

$$\begin{aligned} \varepsilon^{-1} \left( \frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f} \right) h'' - \varepsilon^{-2} h h'' \\ - \left( \frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f} \right) Da^{-1} h' + \varepsilon^{-2} \left( \frac{1}{2} h'^2 - 2g^2 \right) \\ - 2 \frac{\beta_{nf}}{\beta_f} \lambda \theta = 0 \end{aligned} \quad (8)$$

$$\begin{aligned} \varepsilon^{-1} \left( \frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f} \right) g'' - \varepsilon^{-2} (h g' - h' g) \\ - \left( \frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f} \right) Da^{-1} g = 0 \end{aligned} \quad (9)$$

$$\begin{aligned} \frac{1}{Pr} \frac{k_{nf} / k_f}{(\rho C_p)_{nf} / (\rho C_p)_f} \theta'' - h \theta' \\ + \frac{1}{2} h' \theta = 0 \end{aligned} \quad (10)$$

subject to the boundary conditions

$$\left. \begin{aligned} h(0) = 0, h'(0) = 0, g(0) = 1, \theta(0) = 1 \\ h'(\eta) \rightarrow 0, g(\eta) \rightarrow 0, \\ \theta(\eta) \rightarrow 0 \end{aligned} \right\} \text{ as } \eta \rightarrow \infty, \quad (11)$$

where,  $Da^{-1}$  is the inverse Darcy number and  $\lambda$  is the mixed convection parameter, which mathematically expressed as

$$Da^{-1} = \frac{v_f}{K \Omega \sin \alpha}, \lambda = \frac{Gr_L}{Re_L^2} \quad (12)$$

with  $Gr_L = g \beta_f (T_w - T_\infty) \cos \alpha L^3 / v_f^2$  as the Grashof number and  $Re_L = \Omega L^2 \sin \alpha / v_f$  as the Reynolds number. The constant mixed convection parameter is denoted by  $\lambda$  with  $\lambda > 0$  for assisting flow,  $\lambda < 0$  for opposing flow and  $\lambda = 0$  for forced convection flow. The opposing flow will be the main focus.

The skin friction coefficients  $C_{f_x}$ ,  $C_{f_y}$ , and the local Nusselt number  $Nu_x$ , are equated as (Hering & Grosh, 1963):

$$\begin{aligned}
 C_{f,x} &= \frac{2\mu_{nf}}{\rho_f \nu_w^2(x)} \left( \frac{\partial u}{\partial z} \right)_{z=0}, \\
 C_{f,y} &= \frac{2\mu_{nf}}{\rho_f \nu_w^2(x)} \left( \frac{\partial v}{\partial z} \right)_{z=0}, \\
 Nu_x &= -\frac{xk_{nf}}{k_f(T_w - T_\infty)} \left( \frac{\partial T}{\partial z} \right)_{z=0}.
 \end{aligned} \tag{13}$$

Using Eq. (6) and Eq. (13) we get

$$\begin{aligned}
 Re_L^{1/2} C_{f,x} &= -\frac{\mu_{nf}}{\mu_f} h''(0), \\
 2^{-1} Re_L^{1/2} C_{f,y} &= \frac{\mu_{nf}}{\mu_f} g'(0), \\
 Re_L^{-1/2} Nu_x &= -\frac{k_{nf}}{k_f} \theta'(0).
 \end{aligned} \tag{14}$$

### 3. STABILITY ANALYSIS

As two non-identical solutions are perceived to be executed in this study, here, we include the stability analysis to evaluate and validate the feature of the solutions. This analysis has been initiated by Merkin (1986) and extensively followed by other researchers (Khashi'ie *et al.*, 2021; Mabood & Akinshilo, 2021; Tshivhi & Makinde, 2021; Wahid *et al.*, 2021; Yahaya *et al.*, 2021; Kolsi *et al.*, 2021; Aladdin & Bachok, 2021). To analyze the stability, we first need to set Eqs. (2)-(4) to be unsteady and introducing the following newly similarity transformation,

$$\begin{aligned}
 u &= x\Omega \sin \alpha f(\eta, \tau), \\
 v &= x\Omega \sin \alpha g(\eta, \tau), \\
 w &= \sqrt{v_f \Omega \sin \alpha} h(\eta, \tau), \\
 \theta(\eta, \tau) &= \frac{T - T_\infty}{T_w - T_\infty}, \\
 \eta &= z\sqrt{\Omega \sin \alpha / \nu_f}, \quad \tau = t\Omega \sin \alpha
 \end{aligned} \tag{15}$$

where  $\tau$  is the non-dimensional time variable with time  $t$ . Hence, applying this transformation towards the unsteady equations, we then obtain the subsequent form of equations

$$\begin{aligned}
 \varepsilon^{-1} \left( \frac{\mu_{nf} / \mu_f}{\rho_{nf} / \rho_f} \right) \frac{\partial^3 h}{\partial \eta^3} - \varepsilon^{-2} h \frac{\partial^2 h}{\partial \eta^2} \\
 - 2 \frac{\beta_{nf}}{\beta_f} \lambda \theta - \frac{\mu_{nf} / \mu_f}{\rho_{nf} / \rho_f} Da^{-1} \frac{\partial h}{\partial \eta} \\
 - \frac{1}{2} \left( \frac{\partial^2 h}{\partial \eta \partial \tau} \right) + \varepsilon^{-2} \left( \frac{1}{2} \left( \frac{\partial h}{\partial \eta} \right)^2 - 2g^2 \right) = 0
 \end{aligned} \tag{16}$$

$$\begin{aligned}
 \varepsilon^{-1} \left( \frac{\mu_{nf} / \mu_f}{\rho_{nf} / \rho_f} \right) \frac{\partial^2 g}{\partial \eta^2} - \varepsilon^{-2} \left( h \frac{\partial g}{\partial \eta} - \frac{\partial h}{\partial \eta} g \right) \\
 - \left( \frac{\mu_{nf} / \mu_f}{\rho_{nf} / \rho_f} \right) Da^{-1} g - \left( \frac{\partial g}{\partial \tau} \right) = 0
 \end{aligned} \tag{17}$$

$$\begin{aligned}
 \frac{1}{Pr} \frac{k_{nf} / k_f}{(\rho C_p)_{nf} / (\rho C_p)_f} \frac{\partial^2 \theta}{\partial \eta^2} - h \frac{\partial \theta}{\partial \eta} \\
 + \frac{1}{2} \frac{\partial h}{\partial \eta} \theta - \left( \frac{\partial \theta}{\partial \tau} \right) = 0
 \end{aligned} \tag{18}$$

subject to

$$\begin{aligned}
 \left. \begin{aligned}
 h(\eta, \tau) = 0, \quad \frac{\partial h}{\partial \eta}(\eta, \tau) = 0, \\
 g(\eta, \tau) = 1, \quad \theta(\eta, \tau) = 1,
 \end{aligned} \right\} \text{at } \eta = 0 \\
 \left. \begin{aligned}
 \frac{\partial h}{\partial \eta}(\eta, \tau) \rightarrow 0, \quad g(\eta, \tau) \rightarrow 0, \\
 \theta(\eta, \tau) \rightarrow 0
 \end{aligned} \right\} \text{as } \eta \rightarrow \infty
 \end{aligned} \tag{19}$$

According to Weidman *et al.* (2006), the following eigenvalue equations that consist of eigenvalue parameter  $\gamma$  should be applied towards the previous transformed equations in evaluating the stability of the solution,

$$\begin{aligned}
 h(\eta, \tau) &= h_0(\eta) + e^{-\gamma\tau} H(\eta), \\
 g(\eta, \tau) &= g_0(\eta) + e^{-\gamma\tau} G(\eta), \\
 \theta(\eta, \tau) &= \theta_0(\eta) + e^{-\gamma\tau} Q(\eta),
 \end{aligned} \tag{20}$$

where  $H(\eta), G(\eta), Q(\eta)$  are relatively small to  $h(\eta) = h_0(\eta), g(\eta) = g_0(\eta), \theta(\eta) = \theta_0(\eta)$ , separately. Upon simplification, we obtain the linearized eigenvalue system as follows

$$\begin{aligned}
 \varepsilon^{-1} \left( \frac{\mu_{nf} / \mu_f}{\rho_{nf} / \rho_f} \right) H''' - \varepsilon^{-2} (h_0 H'' + H h_0'') \\
 - \left( \frac{\mu_{nf} / \mu_f}{\rho_{nf} / \rho_f} \right) Da^{-1} H' \\
 + \varepsilon^{-2} (h_0' H' - 4g_0 G) - 2 \frac{\beta_{nf}}{\beta_f} \lambda Q + \frac{1}{2} \gamma H' = 0
 \end{aligned} \tag{21}$$

$$\begin{aligned}
 \varepsilon^{-1} \left( \frac{\mu_{nf} / \mu_f}{\rho_{nf} / \rho_f} \right) G'' \\
 - \varepsilon^{-2} ((h_0 G' + H g_0') - (h_0' G + H' g_0)) \\
 - \left( \frac{\mu_{nf} / \mu_f}{\rho_{nf} / \rho_f} \right) Da^{-1} G + \gamma G = 0
 \end{aligned} \tag{22}$$

$$\begin{aligned}
 \frac{1}{Pr} \frac{k_{nf} / k_f}{(\rho C_p)_{nf} / (\rho C_p)_f} Q'' - (h_0 Q' + H \theta_0') \\
 + \frac{1}{2} (h_0' Q + H' \theta_0) + \gamma Q = 0
 \end{aligned} \tag{23}$$

subject to

$$\begin{aligned}
 H(0) = 0, \quad H'(0) = 0, \quad G(0) = 0, \quad Q(0) = 0, \\
 H''(0) = 1 \text{ (additional)} \\
 \left. \begin{aligned}
 H'(\eta) \rightarrow 0 \text{ (rest)}, \\
 G(\eta) \rightarrow 0, \\
 Q(\eta) \rightarrow 0
 \end{aligned} \right\} \text{as } \eta \rightarrow \infty.
 \end{aligned} \tag{24}$$

The stability of the solution is analyzed via the generation of an infinite number of eigenvalues  $\gamma_1 < \gamma_2 < \gamma_3 \dots < \gamma_{n-1} < \gamma_n$  where if  $\gamma_1 > 0$ , we consider the solution as stable, and if  $\gamma_1 < 0$ , the solution is considered as non-stable because of the initial broadening of perturbations. Since all conditions are homogenous, we need to rest one condition and enforce a new additional condition as stated in Eq. (24) to ensure a possible set of eigenvalues can be generated (Harris *et al.*, 2009).

#### 4. NUMERICAL COMPUTATION

The flow problem is resolved using `bvp4c` solver MATLAB. This solver employs a finite difference approach that utilizes the three-stage Lobatto IIIa collocation formula, yielding a continuous solution with fourth-order precision (Kierzenka & Shampine, 2001; Shampine *et al.*, 2003, 2004). The general syntax of the solver is `sol = bvp4c (@OdeBVP, @OdeBC, solinit, options)`. This syntax contains several important functions that contain the main equations, boundary conditions, the initial mesh points and solution approximation, and the optional integration parameter, respectively. The mesh point is used in the collocation method to divide the integration interval into smaller parts. The algorithm for the solver begins with:

- (i) Variable declaration
- (ii) Initialization
- (iii) Domain discretization
- (iv) Call `bvp4c`
- (v) Solution evaluation using Deval function
- (vi) Numerical solutions computation

The residual of the continuous solution is employed to guide mesh selection and error control. If the solution unable to meet the tolerance limit, the solver will modify the mesh and the process will be repeated.

Before utilizing the solver, the resulting equations Eqs. (8)-(10) subject to Eq. (11) should be transformed into first-order differential equations, where we assume  $h = y(1)$ ,  $h' = y(2)$ ,  $h'' = y(3)$ ,  $g = y(4)$ ,  $g' = y(5)$ ,  $\theta = y(6)$  and  $\theta' = y(7)$  so that the resulting equations are rewritten as the following,

$$h''' = \frac{\left( \begin{array}{l} \varepsilon^{-2} y(1)y(3) + \left( \frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f} \right) Da^{-1} y(2) \\ -\varepsilon^{-2} \left( \frac{1}{2} y(2)y(2) - 2y(4)y(4) \right) \\ + 2 \frac{\beta_{nf}}{\beta_f} \lambda y(6) \end{array} \right)}{\left( \frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f} \right)}$$

$$g'' = \frac{\varepsilon}{\left( \frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f} \right)} \left( \begin{array}{l} \varepsilon^{-2} (y(1)y(5) - y(2)y(4)) \\ + \left( \frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f} \right) Da^{-1} y(4) \end{array} \right)$$

$$\theta'' = \frac{1}{\frac{1}{Pr} \left( \frac{k_{nf}}{\rho C_p} \right)_{nf} / \left( \frac{\rho C_p}{k} \right)_f} \left( \begin{array}{l} y(1)y(7) \\ - \frac{1}{2} y(2)y(6) \end{array} \right) \tag{25}$$

subject to

$$\begin{aligned} &ya(1), ya(2), ya(4) - 1, ya(6) - 1, \\ &yb(2), yb(4), yb(6) \end{aligned} \tag{26}$$

where  $ya$  and  $yb$  refer to the boundary conditions when  $\eta = 0$  and  $\eta \rightarrow \infty$ , respectively. The thickness of the boundary layer ( $\eta_\infty = 15$ ), the value of the parameters, and the initial guesses need to be set up accordingly in the coding program to execute the appropriate numerical solutions. The initial guesses are quite important in generating the best solutions because the efficacy of the solver ultimately depends on the appropriateness of the selected initial guesses since this solver is an iterative scheme. The numerical solution is acceptable when it is asymptotically converged towards the boundary conditions, and there is zero warning/error so that the numerical solution complies with the specified tolerance limit.

**Table 3 Comparison values when  $Pr = 7$ ,  $\lambda = Da^{-1} = 0$  in the absence of porosity and MNPs  $\phi = 0$**

|               | Present     | (Rashad <i>et al.</i> , 2016) | (Hering & Grosh, 1963) |
|---------------|-------------|-------------------------------|------------------------|
| $-h''(0)$     | 1.020464858 | 1.0203                        | 1.0205                 |
| $-g'(0)$      | 0.615921901 | 0.61583                       | 0.61592                |
| $-\theta'(0)$ | 0.428545552 | 0.42842                       | 0.42852                |

**Table 4 Comparison values when  $Pr = 1, 2$ ,  $\lambda = 0.1$ ,  $Da^{-1} = 0$  in the absence of porosity and MNPs  $\phi = 0$**

|               | Pr = 1                   | Pr = 2                   |
|---------------|--------------------------|--------------------------|
| $-h''(0)$     | 1.128544651<br>(1.12824) | 1.111471509<br>(1.11203) |
| $-g'(0)$      | 0.648233892<br>(0.64374) | 0.627816846<br>(0.63347) |
| $-\theta'(0)$ | 0.546775247<br>(0.54573) | 0.740985139<br>(0.74502) |

( ) refers to the solution reported by (Rashad *et al.*, 2016)

For validation purposes, the precision of the present method is validated by contrasting the executed numerical solutions with the previous studies for certain limiting cases as can be observed in Tables 3 and 4. The solutions are compared for the case

limited to the absence of porosity parameter and the exclusion of MNP (regular fluid). As tabulated in the tables, the numerical solutions are seen to be aligned with the prior studies although they implement a different kind of method in solving the problem. This comparison shows the trustworthiness and accuracy of the implemented numerical method.

For the computation on conducting the stability analysis, the same procedure is needed to reduce the system of equations where the assumptions and modification are made as follows:

$$\begin{aligned} h_0 &= s(1), h_0' = s(2), h_0'' = s(3), \\ g_0 &= s(4), g_0' = s(5), \theta_0 = s(6), \theta_0' = s(7), \\ H &= y(1), H' = y(2), H'' = y(3), \\ G &= y(4), G' = y(5), Q = y(6), Q' = y(7), \end{aligned}$$

$$H''' = \frac{\begin{pmatrix} \varepsilon^{-2}(s(1)y(3) + y(1)s(3)) \\ + \left(\frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f}\right) Da^{-1}y(2) \\ - \varepsilon^{-2}(s(2)y(2) - 4s(4)y(4)) \\ + 2\frac{\beta_{nf}}{\beta_f} \lambda y(6) - \frac{1}{2}\gamma y(2) \end{pmatrix}}{\left(\frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f}\right)}$$

$$G'' = \frac{\begin{pmatrix} \varepsilon^{-2}\left((s(1)y(5) + y(1)s(5))\right. \\ \left. - (s(2)y(4) + y(2)s(4))\right) \\ + \left(\frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f}\right) Da^{-1}y(4) - \gamma y(4) \end{pmatrix}}{\left(\frac{\mu_{nf}}{\rho_{nf}} / \frac{\mu_f}{\rho_f}\right)}$$

$$Q'' = \frac{1}{\frac{1}{Pr} \left(\frac{k_{nf}}{\rho C_p}\right)_{nf}} \begin{pmatrix} (s(1)y(7) + y(1)s(7)) \\ -\frac{1}{2}s(2)y(6) \\ -\frac{1}{2}y(2)s(6) \\ -\gamma y(6) \end{pmatrix} \frac{1}{(\rho C_p)_f}$$

(27)

subject to

$$\begin{aligned} ya(1), ya(2), ya(4), ya(6), ya(3) - 1, \\ yb(4), yb(6) \end{aligned} \tag{28}$$

### 5. RESULTS AND DISCUSSION

As previously stated, the numerical solutions have been validated with the preceding studies for certain limiting cases, and therefore in this section, we are confident in executing the numerical solutions for the case of MNF with the inclusion of the porosity regime. The MNF contains cobalt ferrite (CoFe<sub>2</sub>O<sub>4</sub>) and is dispersed into the base liquid which is water. This MNF formation (CoFe<sub>2</sub>O<sub>4</sub>-H<sub>2</sub>O) is analyzed in terms of their skin friction and heat transfer performance with several changing parameters. The

thermophysical characteristic of the respective components in the MNF are set as tabulated in Table 2, where the volume fraction of CoFe<sub>2</sub>O<sub>4</sub> is investigated at the amount of 1% to 2%.

Figures 2-4 display the distributions of tangential  $Re_L^{1/2} C_{fx}$  and azimuthal  $2^{-1} Re_L^{1/2} C_{fy}$  skin friction coefficients, and the local Nusselt number  $Re_L^{-1/2} Nu_x$  against the mixed convection ( $\lambda < 0$ ) with a different volume fraction of CoFe<sub>2</sub>O<sub>4</sub>. These distributions are calculated with a fixed value of inverse Darcy number  $Da^{-1} = 0.01$  and porosity parameter  $\varepsilon = 1$  to evaluate the impacts of the volume fraction of CoFe<sub>2</sub>O<sub>4</sub> towards the physical quantities stated. As shown in the figures (Figs. 2-4) by the first solution, this study confirms the ability of MNP (i.e., CoFe<sub>2</sub>O<sub>4</sub>) in improving  $Re_L^{1/2} C_{fx}$  and  $Re_L^{-1/2} Nu_x$  (heat transfer rate) when its dispersion is gradually added towards the base liquid, but not for  $2^{-1} Re_L^{1/2} C_{fy}$ .

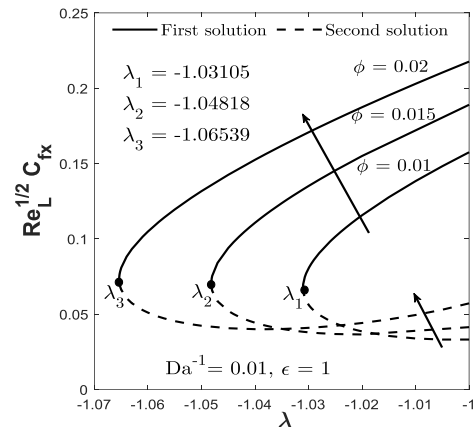


Fig. 2. Distribution of  $Re_L^{1/2} C_{fx}$  for different  $\phi$ .

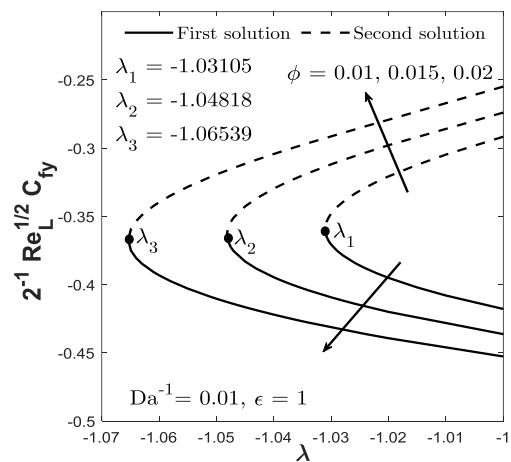
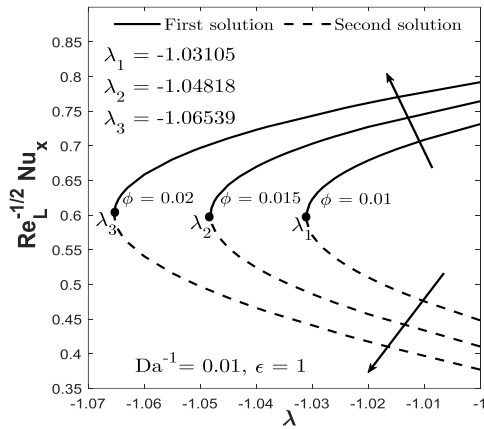


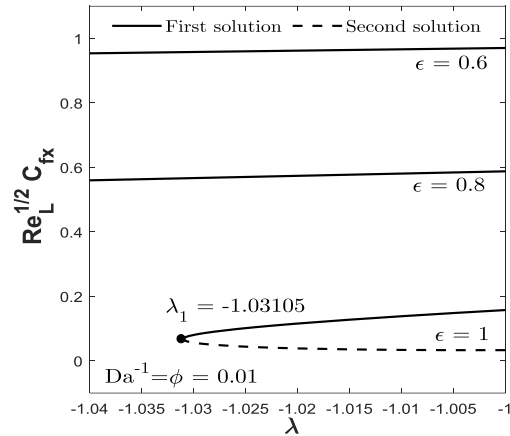
Fig. 3. Distribution of  $2^{-1} Re_L^{1/2} C_{fy}$  for different  $\phi$ .



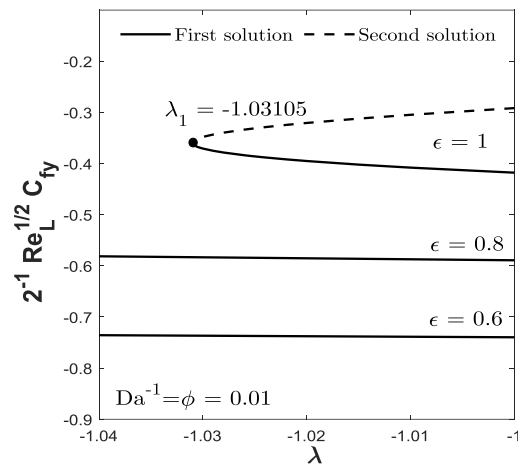
**Fig. 4.** Distribution of  $Re_L^{-1/2} Nu_x$  for different  $\phi$ .

Meanwhile, for the distributions of  $2^{-1} Re_L^{1/2} C_{fy}$  and  $Re_L^{-1/2} Nu_x$  in Figs. 3 and 4, the second solution shows the reflected pattern compared to its respective first solution as the volume fraction of  $CoFe_2O_4$  increases. However, this second solution is validated to be non-stable when we evaluate its stability. The boundary layer separation for this case is seen to be located at the negative region of  $\lambda$  which is when the fluid experiencing the opposing flow due to the mixed convection. In particular, the critical point of the separation process takes place at  $\lambda_{c1} = -1.03105$  ( $\phi = 0.01$ ),  $\lambda_{c2} = -1.04818$  ( $\phi = 0.015$ ) and  $\lambda_{c3} = -1.06539$  ( $\phi = 0.02$ ). Beyond this point, there is no feasible solution appeared. On a side note, this boundary layer separation from the state of laminar to turbulent would cause vibrations and obstruction in machinery and reduce the efficiency of the compressor if we consider it into practice (Gaviln, 2010). Therefore, to prevent such occurrence, this finding suggests increasing the volume fraction of  $CoFe_2O_4$  or the mixed convection parameter accordingly. The flow is only favorable when  $\lambda \geq \lambda_c$ .

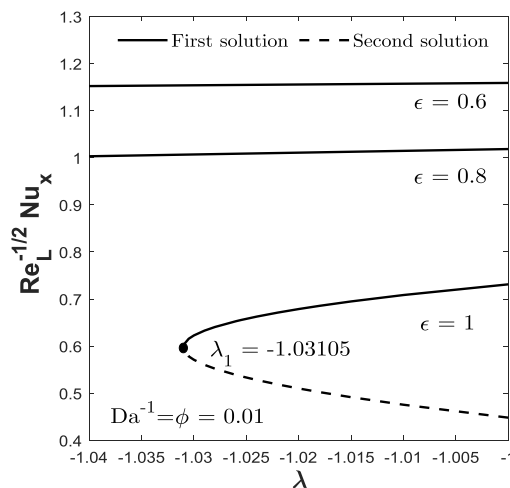
Figures 5-7 demonstrate the distributions of  $Re_L^{1/2} C_{fx}$ ,  $2^{-1} Re_L^{1/2} C_{fy}$  and  $Re_L^{-1/2} Nu_x$ , separately, against  $\lambda (< 0)$  with a different value of  $\epsilon$  when  $\phi = Da^{-1} = 0.01$ . In this case, the smaller value of  $\epsilon$  is more dominant to improve  $Re_L^{1/2} C_{fx}$  and  $Re_L^{-1/2} Nu_x$  as can be contemplated from the first solution. Similar as Figures 2-4, the critical point for the separation process located at  $\lambda_{c1} = -1.03105$  when  $\epsilon = 1$ , while for the case when  $\epsilon = 0.6, 0.8$ , the critical points should be further away ( $\lambda_c < -1.03105$ ). This also implies that the smaller porosity value would delay the separation process even better. The value of  $Re_L^{1/2} C_{fx}$ ,  $2^{-1} Re_L^{1/2} C_{fy}$  and  $Re_L^{-1/2} Nu_x$  can also be



**Fig. 5.** Distribution of  $Re_L^{1/2} C_{fx}$  for different  $\epsilon$



**Fig. 6.** Distribution of  $2^{-1} Re_L^{1/2} C_{fy}$  for different  $\epsilon$

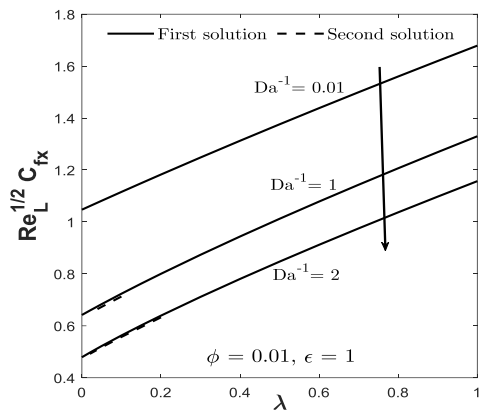


**Fig. 7.** Distribution of  $Re_L^{-1/2} Nu_x$  for different  $\epsilon$

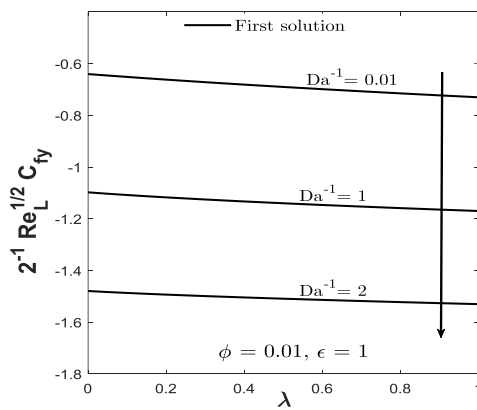
augmented by strengthening the mixed convection parameter for the first solution.



Additionally, the distributions of  $Re_L^{1/2} C_{fx}$ ,  $2^{-1} Re_L^{1/2} C_{fy}$  and  $Re_L^{-1/2} Nu_x$  against  $\lambda(>0)$  for varied  $Da^{-1}$  when  $\phi=0.01$  and  $\epsilon=1$  are shown in Figures 8-10. The increment of inverse Darcy number is contemplated to reduce these distributions which also implies the reduction in  $Re_L^{1/2} C_{fx}$ ,  $2^{-1} Re_L^{1/2} C_{fy}$  and  $Re_L^{-1/2} Nu_x$  when the flow is assisted through the mixed convection. Enlarging  $Da^{-1}$  would depreciate the permeability of the medium which becomes the reason towards such pattern of distribution.



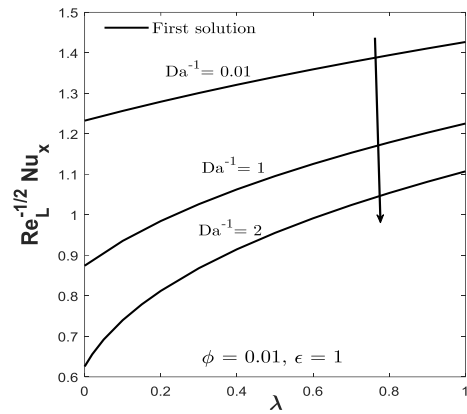
**Fig. 8.** Distribution of  $Re_L^{1/2} C_{fx}$  for different  $Da^{-1}$ .



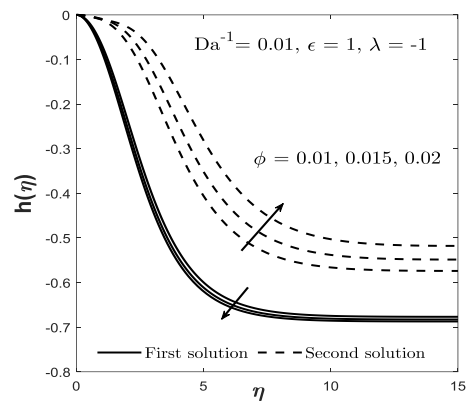
**Fig. 9.** Distribution of  $2^{-1} Re_L^{1/2} C_{fy}$  for different  $Da^{-1}$ .

In Figs. 11-18, we illustrate the impacts of volume fraction of  $CoFe_2O_4$  and porosity parameter towards the three different velocity profiles which are the normal  $h(\eta)$ , tangential  $h'(\eta)$  and circumferential (azimuthal)  $g(\eta)$  velocities due to the cone geometry, and also the temperature profile  $\theta(\eta)$ .

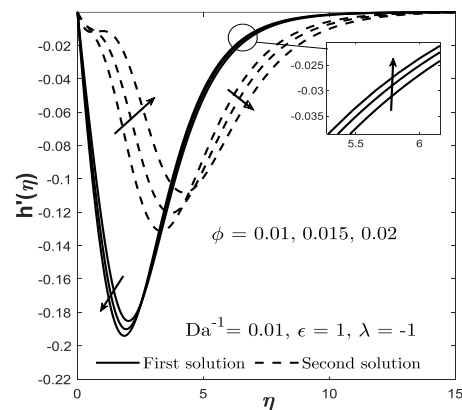
The solutions in these figures suffice the boundary conditions which validate the precision of the



**Fig. 10.** Distribution of  $Re_L^{-1/2} Nu_x$  for different  $Da^{-1}$ .



**Fig. 11.** Distribution of  $h(\eta)$  for different  $\phi$ .



**Fig. 12.** Distribution of  $h'(\eta)$  for different  $\phi$ .

numerical solutions. In the context of the first solution, a more concentrated  $CoFe_2O_4$  is depicted to decelerate all of the distributions but oppositely at a certain range of  $\eta$  for  $h'(\eta)$  which is after the conflicting point,  $\eta \approx 2.58$ . The inclusion of  $CoFe_2O_4$  increases the fluid thermal conductivity; hence this causes the heat transfer to occur more efficiently and reduces the temperature profile. The normal and circumferential velocities also decelerate due to the concentrated amount of  $CoFe_2O_4$  that resists the flow movements.

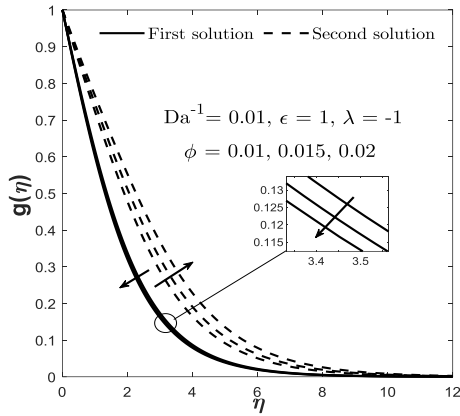


Fig. 13. Distribution of  $g(\eta)$  for different  $\phi$ .

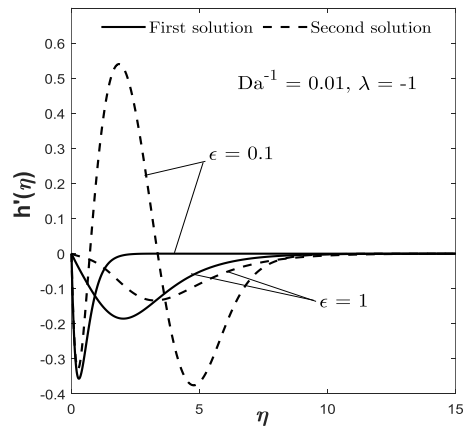


Fig. 16. Distribution of  $h'(\eta)$  for different  $\epsilon$ .

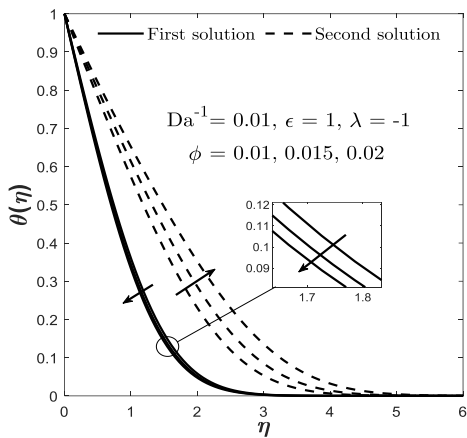


Fig. 14. Distribution of  $\theta(\eta)$  for different  $\phi$ .

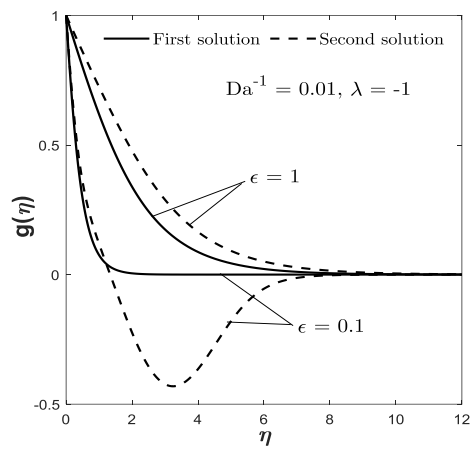


Fig. 17. Distribution of  $g(\eta)$  for different  $\epsilon$ .

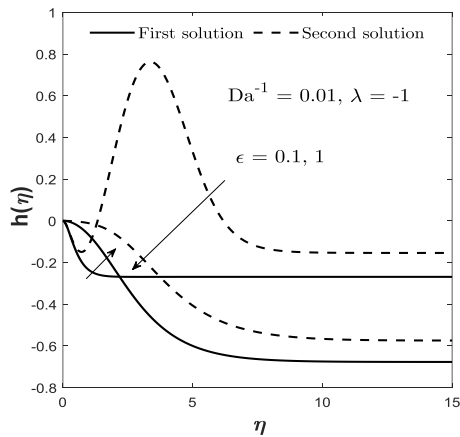


Fig. 15. Distribution of  $h(\eta)$  for different  $\epsilon$ .

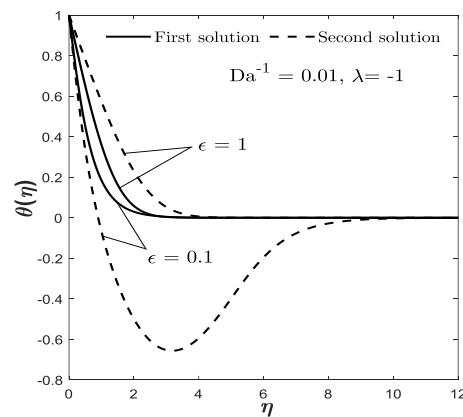
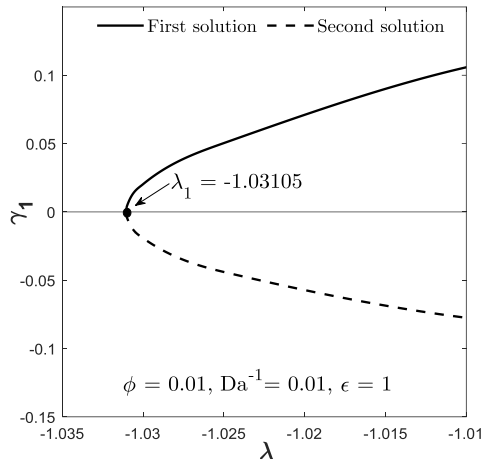


Fig. 18. Distribution of  $\theta(\eta)$  for different  $\epsilon$ .

Since we managed to generate dual solutions, especially for the opposing flow of mixed convection, it is necessary for us to conduct the stability analysis. The findings on the stability analysis is provided in Fig. 19 through the graphical illustration of the smallest eigenvalue  $\gamma_1$  distribution against  $\lambda$  when  $\phi = Da^{-1} = 0.01$ ,  $Pr = 6.96$  and  $\epsilon = 1$ . Initially, we already perceived the first solution to be stable as it is appeared to be the closest solution

towards the boundary than the second solution when we look at the graph of the profiles in Figs. 11-18. However, this contemplation needs to be validated sophisticatedly by generating the possible eigenvalues through a stability analysis. In Fig. 19, clearly, the first solution is stable as the generated smallest eigenvalue is positive due to the deterioration of perturbation. This analysis is also valid because as  $\lambda \rightarrow \lambda_c$ ,  $\gamma_1 \rightarrow 0$ , meaning that, the perturbation is



**Fig. 19. Distribution of  $\gamma_1$  against  $\lambda$ .**

eventually decayed as time evolves for the stable solution.

Finally, although the incrementation of  $\text{CoFe}_2\text{O}_4$  volume fraction up to 2% is estimated to augment the heat transfer rate as stated previously, the required work for the rotating cone is also increased due to the incrementation of the skin frictions which would result in a higher cost. Therefore, to achieve the optimum heat transfer performance, a ratio of change in the heat transfer rate to change in friction factor or also known as Thermal Performance Factor (TPF) is calculated to approximate the optimum required value for the  $\text{CoFe}_2\text{O}_4$  volume fraction. The mathematical relation of TPF is expressed as follows (Kumar *et al.*, 2016; Maradiya *et al.*, 2018):

$$TPF = \frac{(Nu_x / Nu_{x0})}{(f_c / f_{c0})^{1/3}} \quad (29)$$

where the terms with subscript 0 denotes the respective initial value for the Nusselt number and friction factor. As we observed on our findings (refer Table 5), the TPF value is slightly higher when 1.5% volume fraction of  $\text{CoFe}_2\text{O}_4$  is used compared to 2%. Hence, to have a lesser penalty of the required rotating work when increasing the volume fraction of  $\text{CoFe}_2\text{O}_4$  in regard to augmenting the heat transfer, 1.5% volume fraction is preferable.

**Table 5 TPF value due to the increment of  $\phi$  when  $\lambda = -1$ ,  $\epsilon = 1$  and  $Da^{-1} = 0.01$**

| $\phi$ | 1% to 1.5% | 1% to 2% |
|--------|------------|----------|
| TPF    | 0.984      | 0.972    |

## 6. CONCLUSION

The boundary layer flow and heat transfer of mixed convection MNF past a rotating vertical cone in a variable porosity regime have been scrutinized numerically. Stability analysis is also reported to

complete the investigation. Based on the discussed findings, focusing on the opposing flow, we may conclude that:

- The heat transfer efficiency of the MNF can be magnified by controlling the volume fraction of MNP, mixed convection parameter, and porosity parameter.
- The ability of cobalt ferrite MNP in enhancing the heat transfer efficiency of MNF is proven in this study.
- The presence of a porosity regime increases the temperature of the MNF in the rotating cone and thickens the boundary layer thickness which causes the heat transfer rate to decrease.
- The transition of the boundary layer can be hindered by magnifying the volume fraction of MNP.
- Higher mixed convection magnifies the heat transfer, and the skin friction rates.
- The opposing flow of the mixed convection made the separation point of the boundary layer discoverable, and the existence of an alternative solution can be revealed.
- The alternative (second) solution is non-stable; hence the findings from this solution are not being recommended.

It should be noted that these present findings are only based on the respective MNF. For further investigation, other types of MNP such as magnetite and manganese-zinc ferrite can also be considered in the water/ethylene/methanol-based to analyze their flow and heat transfer behavior within the same geometry.

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