

A Model for Predicting Post-Stall Behavior of Axial Compressors

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ABSTRACT

The current paper reports on a new theory developed by modifying the basic Moore-Greitzer model, which can predict the performance of a compression system during the instabilities in more details. The general assumptions such as the compression system layout, the lags in the entrance and exit ducts, the compressor axisymmetric characteristic and the small disturbances are similar to those of Moore-Greitzer model. However, a second order hysteresis is used in the current work for the pressure rise of the rotor and stator rows. As a result, some new parameters are added to the governing equations, such as the stall cell acceleration ($d^2r/d\xi^2$), second derivative of the mean axial flow coefficient ($d^2\Phi/d\xi^2$), second derivative of the disturbance amplitude ($d^2A/d\xi^2$) and slope of the compressor characteristic curve. This gives the modified model new capabilities, like investigating the transient speed of the stall cell or the effect of the throttling rate on the instabilities, which are discussed in details in the current paper.

Keywords: Surge; Rotating stall; Compressor characteristic.

NOMENCLATURE

a_n, b_n	Fourier coefficient of $g(\theta)$ and $h(\theta)$	m	parameter defining lag tendency outside compressor
A	amplitude function of first-harmonic angular disturbance	N	number of stages of core compressor
A_c	compressor duct area	n	wave number (corresponding to number of stall cells)
a	reciprocal time-lag parameter of blade passage	P	pressure coefficient
a_s	sound speed	p_0	static pressure at entrance to IGV
B	Greitzer parameter	p_1	static pressure at entrance of core compressor
F	steady pressure rise coefficient in blade passage	p_E	static pressure at exit of core compressor
F_T	throttle characteristic function	p_S	static pressure at end of exit duct, and pressure in the plenum
f	non-dimensional speed coefficient	p_T	total pressure ahead of entrance and following the throttle duct
g	disturbance of axial flow coefficient	R	mean wheel radius
H	semi-height of cubic axisymmetric characteristic	r	time-dependent phase angle
h	circumferential velocity coefficient	t	time
K_G	loss coefficient at IGV entrance	U	wheel speed at mean diameter
K_T	throttle coefficient	V_P	volume of plenum
l_c	total aerodynamic length of compressor and ducts	W	semi-width of cubic characteristic
l_E	length of exit in wheel radii	Y	disturbance potential at compressor entrance
l_I	length of entrance in wheel radii		
l_T	length of throttle ducts in wheel radii		

η	axial disturbances measured in wheel radii	θ and ξ	
θ	angular coordinate around wheel	$\tilde{\phi}$	velocity potential in entrance duct
θ^*	angular coordinate around wheel, measured relative to a rotating-stall cell	$\tilde{\phi}'$	disturbance velocity potential
ξ	time, referred to time for wheel to rotate one radian	Ψ	total-to-static pressure rise coefficient
τ	coefficient of pressure-rise lag	ψ_c	axisymmetric pressure rise coefficient
Φ	axial flow coefficient in compressor, annulus averaged; axial velocity divided by wheel speed	ψ_{c0}	shut-off value of axisymmetric characteristic
Φ_T	flow coefficient of throttle duct	SUBSCRIPTS	
ϕ	local axial flow coefficient, a function of	0	at the entrance to the compressor
		E	at the exit of the compressor

1. INTRODUCTION

There is always a strong motivation to increase the safe operating range of axial compressors which is limited by the onset of two aerodynamic instabilities, rotating stall and surge. Surge is characterized as large amplitude oscillations of the annulus flow through the whole compression system, whereas rotating stall is a localized disturbance which might be limited to some of the compressor stages. There are two well-known types of stall inception patterns, modal and spike (McDougall *et al.* (1990) and Day (1993b)). In modal stall inception, long length-scale perturbations gradually buildup and lead to the formation of stall cells. Modal waves might survive 20-200 rotor revolutions prior to rotating stall. This type of stall inception was first predicted theoretically by Moore (1984 I, II) and Moore and Greitzer (1986) before being observed by a number of researchers (e.g., Tryfonidis *et al.* (1995), Garnier *et al.* (1991) and Hendricks (1993)). As reported by Garnier *et al.* (1991) and Hendricks *et al.* (1993), modal stall inception can occur in high speed compressors as well as low speed ones. Furthermore, it was shown by Hendricks *et al.* (1993) that compressibility does not have a dominant effect on the dynamic behavior of the stall cells. On the other hand, spike-type stall inception involves a short length-scale disturbance which appears suddenly and develops directly into rotating stall (Camp and Day (1997) and Gong *et al.* (1999)).

Theoretical and semi-empirical models of surge and rotating stall have been reported by a number of researchers (Moore (1984 I, II), Moore and Greitzer (1986), Emmons (1955), Stenning and Kriebel (1956), Takata and Nagano (1972), Cumpsty and Greitzer (1982)). Emmons (1955) postulated a theory to predict the propagation speed of the stall cell in cascades. Irrotational flow was assumed at the cascade inlet and a transient velocity field (time-averaged axial and tangential velocity components together with small disturbance velocities) was applied. Stenning and Kriebel (1956) also employed small disturbance approach to calculate the stall cell propagation velocity. Takata and Nagano (1972) reported on a nonlinear

analysis of rotating stall, in which blade rows were replaced by semi-actuator disks. A semi-empirical model was presented by Cumpsty and Greitzer (1982), based on an analytical estimate of the pressure change across a stall cell boundary. Moore (1984a, b) developed a model of unsteady pressure rise across a blade passage at in-stall condition. The stall cell was modeled as a small circumferential disturbance to axial and tangential velocities. The disturbances were assumed to be expressed as Fourier series and the propagation velocity of the stall cell was calculated by equating the coefficients of trigonometric functions. A theory was developed by Moore and Greitzer (1986) to model the performance of an axial flow compressor as it leaves stable operation and moves toward instabilities. This model focused on the initial transient period leading to either fully developed rotating stall or surge.

Gong *et al.* (1991) presented a 3-D computational model for compressor instability which employed a three dimensional distribution of body forces. The model made it possible to simulate both modal and spike stall inception. A three dimensional model based on the body force method and empirical correlations has been developed by Righi *et al.* (2018). Results showed that the model can simulate rotating stall and surge fairly accurately.

Many numerical investigations concerning rotating stall inception have been reported recently. Vo *et al.* (2008) introduced two criteria for spike type rotating stall inception. The first condition was that the interface between the tip clearance and oncoming flows becomes parallel to the leading-edge plane, leading to the occurrence of the leading-edge vortex spillage. The second condition was the initiation of reverse flow at the trailing-edge plane. Similar findings were reported for high-speed compressors (e.g., Chen *et al.* (2008), Choi *et al.* (2011) and Khaleghi (2015)). In the experiments reported by Weichert and Day (2013), however, no spillage was observed before and during the emergence of spike. As emphasized by Weichert and Day (2013), the debate about whether forward spillage occurs before or after stall onset is a topic of current interest which requires more numerical and experimental investigations.

Epstein *et al.* (1989) was the first who suggested

the concept of the so called intelligent engines, in which stalling disturbances are detected and suppressed at early stages of formation (e.g., Day (1993a) and Paduano *et al.* (1991)). Since then Moore-Greitzer model has become a theoretical framework for active control of instabilities in compression systems. However, there are some drawbacks in the basic Moore-Greitzer model, one of which is that it does not include the slope of the compressor characteristic curve (it is assumed that stall is initiated at peak pressure rise where the slope of the compressor characteristic is zero). However, Camp and Day (1997) showed that the slope of the compressor total to static pressure rise characteristic for modal stall inception can be between roughly -0.2 to +0.2. Furthermore, the basic Moore-Greitzer method can not model the transient behavior of the stall cells. The main objective of the current work is to develop a modified model based on the basic Moore-Greitzer method with more capabilities and advantages such as modeling the stall cell transient behavior and including the slope of the compressor characteristic curve for low-speed axial compressor.

2. MODELING

2.1 Compressor Model

The compression system is assumed to be the same as that modeled by Moore and Greitzer (1986) (Fig. 1 in Moore and Greitzer (1986)). The compressor is assumed to have high hub-to-tip radius ratio blades, which enables 2-D flow assumption. The inlet and outlet channels as well as the compressor are assumed to have constant cross sections. The flow is assumed to be incompressible, frictionless and irrotational within the entrance duct. It is further assumed that the flow is inviscid throughout the whole compression system and also is compressible everywhere, except in the plenum chamber. The circumferential coordinate is denoted by the wheel angle θ and the axial coordinate by the non-dimensional parameter η (the axial distance divided by the compressor mean radius). Furthermore, the non-dimensional time is defined as:

$$\xi = Ut / R \quad (1)$$

The axial flow coefficient is postulated to be consisted of a mean value and a small axial disturbance (Eq. (2)). This axial disturbance term is not only a function of the circumferential coordinate but also a function of time, in order to enable transient behavior of the compression system during surge or stall.

$$\phi = \Phi(\xi) + g(\xi, \theta) \quad (2)$$

The mean axial flow coefficient ($\Phi(\xi)$) is defined as:

$$\frac{1}{2\pi} \int_0^{2\pi} \phi(\xi, \theta) d\theta = \Phi(\xi) \quad (3)$$

A circumferential disturbance is necessary to

satisfy the continuity:

$$h = h(\xi, \theta) \quad (4)$$

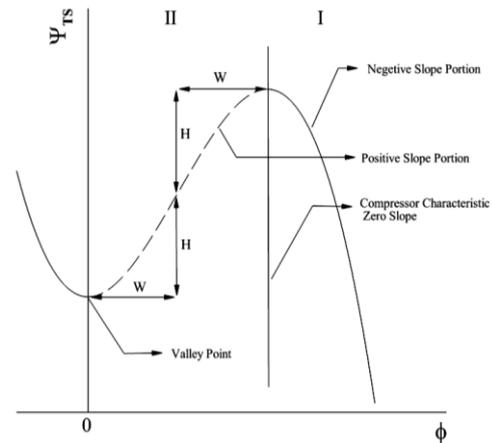


Fig. 1. Compressor axisymmetric characteristic.

As mentioned above, Φ is the circumferential average of ϕ , and therefore, the angle average of g must be vanished. Furthermore, due to the irrotational assumption at the entrance of the compressor, the angle average of the circumferential disturbance (h) must be vanished:

$$\int_0^{2\pi} g(\xi, \theta) d\theta = 0; \quad \int_0^{2\pi} h(\xi, \theta) d\theta = 0 \quad (5)$$

In the recent work done by Khaleghi *et al.* (2020) and Shahriyari *et al.* (2019), the compressor pressure rise function which was used by Moore (1984a) and Moore and Greitzer (1986) was modified to include a second order derivative term, which enabled the investigation of the stall cell transient behavior. The same hypothesized function is used in the current study:

$$\frac{\Delta p}{\frac{1}{2} \rho U^2} = F(\phi) - \tau \left(\frac{d\phi}{dt} + \frac{d^2\phi}{dt^2} \right) \quad (6)$$

The terms $d\phi/dt$ and $d^2\phi/dt^2$ for the rotor and stator can be expressed as follows:

$$\left(\frac{d\phi}{dt} \right)_{stator} = \frac{U}{R} \frac{\partial \phi}{\partial \xi} \quad (7)$$

$$\left(\frac{d\phi}{dt} \right)_{rotor} = \frac{U}{R} \left(\frac{\partial \phi}{\partial \xi} + \frac{\partial \phi}{\partial \theta} \right) \quad (8)$$

$$\left(\frac{d^2\phi}{dt^2} \right)_{stator} = \left(\frac{U}{R} \right)^2 \frac{\partial^2 \phi}{\partial \xi^2} \quad (9)$$

$$\left(\frac{d^2\phi}{dt^2} \right)_{rotor} = \left(\frac{U}{R} \right)^2 \left(\frac{\partial^2 \phi}{\partial \xi^2} + 2 \frac{\partial^2 \phi}{\partial \xi \partial \theta} + \frac{\partial^2 \phi}{\partial \theta^2} \right) \quad (10)$$

By putting Eqs. (7-10) into Eq. (6) and applying the same model for all of the stages, the pressure rise coefficient for the N-stage compressor becomes:

$$\frac{p_E - p_1}{\rho U^2} = NF(\phi) - \frac{1}{2a} \left(2 \frac{\partial \phi}{\partial \xi} + \frac{\partial \phi}{\partial \theta} \right) - \frac{1}{2a} \left[\frac{U}{R} \left(2 \frac{\partial^2 \phi}{\partial \xi^2} + 2 \frac{\partial^2 \phi}{\partial \xi \partial \theta} + \frac{\partial^2 \phi}{\partial \theta^2} \right) \right] \quad (11)$$

$$a = \frac{R}{N\tau U} \quad (12)$$

2.2 Inlet Guide Vanes

Similar to Moore and Greitzer (1986) and using the same assumptions, the pressure rise through the inlet guide vanes can be modeled as:

$$\frac{p_1 - p_0}{\rho U^2} = \frac{1}{2} K_G h^2 \quad (13)$$

Where the term $K_G h^2$ is the coefficient of abrupt pressure rise at the IGV entrance. Note that if the IGV has no loss, the value of K_G will be equivalent to one, and otherwise, less than one.

2.3 Entrance Duct

The flow in the entrance duct is assumed to be inviscid, incompressible and irrotational, and therefore, Laplace Equation can be used. A velocity potential function ($\tilde{\phi}$) is defined, the derivatives of which gives the axial flow coefficient (ϕ) and the circumferential disturbance (h):

$$\left(\tilde{\phi}_\eta \right)_0 = \Phi(\xi) + g(\xi, \theta); \quad \left(\tilde{\phi}_\theta \right)_0 = h(\xi, \theta) \quad (14)$$

The velocity potential function is defined by Eq. (15) so that it satisfies the condition that $\tilde{\phi}$ be equal to zero at the entrance of the compression system (reservoir).

$$\tilde{\phi} = (\eta + l_I) \Phi(\xi) + \tilde{\phi}'(\xi, \eta) \quad (15)$$

In order to determine $\tilde{\phi}$, the velocity potential function for the disturbances ($\tilde{\phi}'$) must be defined, which is given by Eq. (17) (it satisfies the Laplace equation given in Eq. (16)). The derivatives of this Equation in the directions of η and θ at the compressor face are equal to g and h , respectively. Furthermore, note that this velocity potential function is vanished at far upstream.

$$\tilde{\phi}'_{\theta\theta} + \tilde{\phi}'_{\eta\eta} = 0 \quad (16)$$

$$\tilde{\phi}' = \sum_{n=1}^{\infty} \frac{1}{n} e^{n\eta} (a_n \sin n\theta + b_n \cos n\theta), \quad \eta \leq 0 \quad (17)$$

By applying the Bernoulli Equation between far upstream and the compressor face (See Moore and Greitzer (1986)).

$$\frac{p_T - p_0}{\rho U^2} = \frac{1}{2} (\phi^2 + h^2) + \left(\tilde{\phi}'_\xi \right)_0 \quad (18)$$

Where:

$$\left(\tilde{\phi}'_\xi \right)_0 = l_I \frac{d\Phi}{d\xi} + \left(\phi'_\xi \right)_0 \quad (19)$$

2.4 Outlet Guide Vanes and Exit Duct

The pressure rise of the OGV and exit duct can be modeled as follows (see Eqs. (17-20) in Moore and Greitzer (1986)):

$$\frac{p_s - p_E}{\rho U^2} = (p_E) = -l_E \frac{d\Phi}{d\xi} - (m-1) \left(\tilde{\phi}'_\xi \right)_0 \quad (20)$$

Where m is the compressor lag parameter and its value is between one and two (see Moore (1984a)).

2.5 Pressure Rise through the Compression System

By using Eqs. (11), (13), (19) and (20), the overall pressure rise through the compressor becomes as follows:

$$\begin{aligned} \frac{p_s - p_T}{\rho U^2} = & \left(NF - \frac{1}{2} \phi^2 \right) - \\ & \left(l_I + \frac{1}{a} + l_E \right) \frac{d\Phi}{d\xi} - \frac{U}{Ra} \frac{d^2\Phi}{d\xi^2} - m \left(\tilde{\phi}'_\xi \right)_0 \\ & - \frac{1}{2a} \left(2\tilde{\phi}'_{\xi\eta} + \tilde{\phi}'_{\theta\eta} \right)_0 - \frac{1}{2} (1 - K_G) h^2 \\ & - \frac{1}{2a} \left[2\tilde{\phi}'_{\xi\eta} + \tilde{\phi}'_{\theta\eta} + \frac{U}{R} \left(2\tilde{\phi}'_{\xi\xi\eta} + 2\tilde{\phi}'_{\xi\theta\eta} + \tilde{\phi}'_{\theta\theta\eta} \right) \right] \end{aligned} \quad (21)$$

From the definitions of the upstream total to downstream static pressure rise coefficient ($\Psi(\xi)$ given in Eq. (22)), the axisymmetric compressor characteristic ($\psi_c(\phi)$ given in Eq. (23)) and the compressor non-dimensional effective length (given in Eq. (24)), Eq. (25) can be obtained. It should be noted that the IGV is assumed to have no loss ($K_G = 1$).

$$\Psi(\xi) \equiv \frac{p_s - p_T}{\rho U^2} \quad (22)$$

$$\psi_c(\phi) = NF - \frac{1}{2} \phi^2 \quad (23)$$

$$l_c = l_I + \frac{1}{a} + l_E \quad (24)$$

$$\begin{aligned} \Psi(\xi) = & \psi_c \left(\Phi + \left(\tilde{\phi}'_\eta \right)_0 \right) - l_c \frac{d\Phi}{d\xi} - \frac{U}{Ra} \frac{d^2\Phi}{d\xi^2} \\ & - m \left(\tilde{\phi}'_\xi \right)_0 - \frac{1}{2a} \left(2\tilde{\phi}'_{\xi\eta} + \tilde{\phi}'_{\theta\eta} \right)_0 \\ & - \frac{1}{2a} \left[2\tilde{\phi}'_{\xi\eta} + \tilde{\phi}'_{\theta\eta} + \frac{U}{R} \left(2\tilde{\phi}'_{\xi\xi\eta} + 2\tilde{\phi}'_{\xi\theta\eta} + \tilde{\phi}'_{\theta\theta\eta} \right) \right] \end{aligned} \quad (25)$$

As Eq. (5) indicated, the circumferential average of the disturbance functions (g and h which are assumed to be periodic) are vanished over 0 to 2π . By taking the first term of the Fourier series given in Eq. (17), the following equation is obtained:

$$\left(\tilde{\phi}'_\eta \right)_0 = - \left(\tilde{\phi}'_{\theta\theta} \right)_0 \quad (26)$$

The function Y is define as follows for the sake of simplicity (see Eqs. (31) to (35) in Moore and Greitzer (1986)):

$$h = Y_\theta; \quad g = -Y_{\theta\theta} \quad (27)$$

It should be noted that Y is periodic ($Y(\xi, \theta + 2\pi) = Y(\xi, \theta)$) and because the cyclic integral of g and h are vanished, the cyclic integral of Y must be vanished as well:

$$\int_0^{2\pi} Y(\xi, \theta) d\theta = 0 \quad (28)$$

By using Eq. (27), Eq. (25) become as follows:

$$\begin{aligned} \Psi(\xi) = & \psi_c(\Phi - Y_{\theta\theta}) - l_c \frac{d\Phi}{d\xi} - \frac{U}{Ra} \frac{d^2\Phi}{d\xi^2} \\ & - mY_\xi + \frac{1}{2a} (2Y_{\xi\theta\theta} + Y_{\theta\theta\theta}) \\ & + \frac{U}{2Ra} [2Y_{\xi\xi\theta\theta} + 2Y_{\xi\theta\theta\theta} + Y_{\theta\theta\theta\theta}] \end{aligned} \quad (29)$$

2.6 Overall Pressure Balance

The continuity equation of the plenum chamber under assumptions of one dimensional and inviscid flow leads to the following equation (Moore and Greitzer (1986)).

$$l_c \frac{d\Psi}{d\xi} = \frac{1}{4B^2} [\Phi(\xi) - \Phi_T(\xi)] \quad (30)$$

In this equation B is the Greitzer parameter:

$$B \equiv \frac{U}{2a_s} \sqrt{\frac{V_p}{A_c l_c}} \quad (31)$$

Where a_s is the speed of sound, V_p is the plenum volume and A_c is the compressor cross sectional area.

$$F_T = \frac{1}{2} K_T \Phi_T^2 \quad (32)$$

Where F_T is the throttle characteristic function and K_T is the throttle coefficient.

One more equation is needed to be solved together with Eqs. (29) and (30) in order to find the unknowns: $\Psi(\xi)$, $\Phi(\xi)$ and $Y(\xi, \theta)$. This equation is obtained by integrating Eq. (29) with respect to θ and using Eq. (28):

$$\begin{aligned} \Psi(\xi) + l_c \frac{d\Phi}{d\xi} + \frac{U}{Ra} \frac{d^2\Phi}{d\xi^2} = \\ \frac{1}{2\pi} \int_0^{2\pi} \Psi_c(\Phi - Y_{\theta\theta}) d\theta \end{aligned} \quad (33)$$

For pure rotating stall, the time derivatives in the above Equations vanish. By applying the change of variable given in Eq. (34), the governing equations

for pure rotating stall become as given in Eqs. (35) to (37). Note that the frame of reference attached to the stall cell is inertia due to the fully developed stall assumption.

$$Y(\xi, \theta) = Y(\theta^*), \quad \text{where } \theta^* = \theta - f\xi \quad (34)$$

$$\begin{aligned} \frac{U}{2Ra} (2f^2 - 2f + 1) \frac{d^4 Y}{d\theta^{*4}} + \\ \frac{1}{2a} (-2f + 1) \frac{d^3 Y}{d\theta^{*3}} \\ + mf \frac{dY}{d\theta^*} = \left[\Psi - \psi_c \left(\Phi - \frac{d^2 Y}{d\theta^{*2}} \right) \right] \end{aligned} \quad (35)$$

$$\Psi = \frac{1}{2\pi} \int_0^{2\pi} \Psi_c \left(\Phi - \frac{d^2 Y}{d\theta^{*2}} \right) d\theta^* \quad (36)$$

$$\Phi = \Phi_T \quad (37)$$

Equation 37 shows that the operating point in pure rotating stall should be on the throttle characteristic curve. Furthermore, note that $dY/d\theta^* = h$ and $d^2 Y/d\theta^{*2} = -g$. By approximating

$\psi_c \left(\Phi - d^2 Y/d\theta^{*2} \right)$ by the first two terms of its

Taylor series (noting that modal waves can be well described by a linear theory Gong (1999)) and representing g and h by Fourier series and taking the first term (so that $dh/d\theta = -g$ similar to Moore (1984a)), Eq. (35) becomes:

$$\frac{U}{2Ra} (2f^2 - 2f + 1) = -\psi'_c \quad (38)$$

$$f = \frac{1/2}{1 + am} \quad (39)$$

By putting Eq. (39) into Eq. (38) the following result is obtained (this equation is valid for the negative slope portion of the compressor characteristic where the parameter a is negative (see Fig. 1) :

$$\psi'_c = \frac{-U}{2Ra} Z \quad (40a)$$

In the positive slope part of the characteristic, a is positive and the following equation can be written:

$$\psi'_c = \frac{U}{2Ra} Z \quad (40b)$$

Where Z is defined for convenience as:

$$Z = \left(1 - \frac{am + 1/2}{(1 + am)^2} \right) \quad (41)$$

By putting Eq. (40) into Eqs. (29) and (33) (Eq. (40(a)) or (40(b)) depending on the operating point), the following equations are obtained (the upper signs in these equations refer to the negative

and the lower ones to the positive part of the compressor characteristic):

$$\Psi(\xi) + l_c \frac{d\Phi}{d\xi} \mp \frac{2\psi'_c}{Z} \frac{d^2\Phi}{d\xi^2} = \psi_c(\Phi - Y_{\theta\theta}) - mY_\xi + \frac{1}{2a}(2Y_{\xi\theta\theta} + Y_{\theta\theta\theta}) \mp \frac{\psi'_c}{Z} [2Y_{\xi\xi\theta\theta} + 2Y_{\xi\theta\theta\theta} + Y_{\theta\theta\theta\theta}] \quad (42)$$

$$\Psi(\xi) + l_c \frac{d\Phi}{d\xi} \mp \frac{2\psi'_c}{Z} \frac{d^2\Phi}{d\xi^2} = \frac{1}{2\pi} \int_0^{2\pi} \Psi_c(\Phi - Y_{\theta\theta}) d\theta \quad (43)$$

$$l_c \frac{d\Psi}{d\xi} = \frac{1}{4B^2} [\Phi(\xi) - F_T^{-1}(\xi)] \quad (44)$$

The three equations derived so far are the momentum of the compression system, the annulus averaged momentum balance and the mass balance of the plenum chamber (Eqs. (42-44)). These equations can be compared to Eqs. (42-44) in Moore and Greitzer (1986). Equation (44) (mass balance of the plenum chamber) is the same as its counterpart in Moore and Greitzer (1986). However, as compared to the basic Moore-Greitzer equations, four terms are added to Eq. (42) and one term to Eq. (43), all of which include the slope of the compressor axisymmetric characteristic (ψ'_c). In order to solve the above equations, an axisymmetric characteristic function ($\psi_c(\phi)$) should be determined for the compressor. The same characteristic function used by Moore and Greitzer (1986) is used in the current study to enable comparison with the basic Moore-Greitzer model (Fig. 1):

$$\psi_c(\phi) = \psi_{c0} + H \left[1 + \frac{3}{2} \left(\frac{\phi}{W} - 1 \right) - \frac{1}{2} \left(\frac{\phi}{W} - 1 \right)^3 \right] \quad (45)$$

Similar to Moore and Greitzer (1986), Galerkin method is used in the current study to solve the above nonlinear equations. The following function is used to represent Y :

$$Y = WA(\xi) \sin(\theta - r(\xi)) \quad (46)$$

Where $A(\xi)$ is the unknown amplitude of the disturbances and $r(\xi)$ is the unknown phase angle (which identifies the variation in angular location of the disturbances). By putting Eq. (46) into Eqs. (42) and (43) and then applying the Galerkin method, the following results are obtained:

$$\frac{1}{2\pi} \int_0^{2\pi} \psi_c(\Phi + WA \sin \xi) d\xi = \Psi + l_c \frac{d\Phi}{d\xi} \mp \frac{2\psi'_c}{Z} \frac{d^2\Phi}{d\xi^2} \quad (47)$$

$$\frac{1}{\pi W} \int_0^{2\pi} \sin \xi \psi_c(\Phi + WA \sin \xi) d\xi = \mp \frac{2\psi'_c}{Z} \frac{d^2A}{d\xi^2} + \left(m + \frac{1}{a} \right) \frac{dA}{d\xi} + \left(\pm \frac{2\psi'_c}{Z} \left(\frac{dr}{d\xi} \right)^2 \mp \frac{2\psi'_c}{Z} \frac{dr}{d\xi} \pm \frac{\psi'_c}{Z} \right) A \quad (48)$$

$$\frac{1}{\pi W} \int_0^{2\pi} \cos \xi \psi_c(\Phi + WA \sin \xi) d\xi = \pm \frac{2\psi'_c}{Z} A \frac{d^2r}{d\xi^2} + \left(\pm \frac{4\psi'_c}{Z} \frac{dA}{d\xi} - mA - \frac{1}{a} A \right) \frac{dr}{d\xi} + \left(\frac{1}{2a} A \mp \frac{2\psi'_c}{Z} \frac{dA}{d\xi} \right) \quad (49)$$

Note that the integral on the left hand side of Eq. (49) becomes zero over a cycle. Unlike the basic Moore-Greitzer, ($dr/d\xi$) is not constant in the current model.

By using Eq. (45) as the axisymmetric characteristic function of the compressor, the final governing equations are obtained:

$$\frac{d\Psi}{d\xi} = \frac{W/H}{4B^2} \left[\frac{\Phi}{W} - \frac{1}{W} F_T^{-1}(\Psi) \right] \frac{H}{l_c} \quad (50)$$

$$\mp \frac{2\psi'_c}{Z} \frac{d^2\Phi}{d\xi^2} + l_c \frac{d\Phi}{d\xi} = \left[-\frac{\Psi - \psi_{c0}}{H} + 1 + \frac{3}{2} \left(\frac{\Phi}{W} - 1 \right) \left(1 - \frac{1}{2} A^2 \right) - \frac{1}{2} \left(\frac{\Phi}{W} - 1 \right)^3 \right] H \quad (51)$$

$$\mp \frac{2\psi'_c}{Z} \frac{d^2A}{d\xi^2} + \left(m + \frac{1}{a} \right) \frac{dA}{d\xi} + \left(\pm \frac{2\psi'_c}{Z} \left(\frac{dr}{d\xi} \right)^2 \mp \frac{2\psi'_c}{Z} \frac{dr}{d\xi} \pm \frac{\psi'_c}{Z} \right) A = \quad (52)$$

$$\frac{3}{2} \frac{AH}{W} \left[1 - \left(\frac{\Phi}{W} - 1 \right)^2 - \frac{1}{4} A^2 \right] \pm \frac{2\psi'_c}{Z} A \frac{d^2r}{d\xi^2} + \left(\pm \frac{4\psi'_c}{Z} \frac{dA}{d\xi} - mA - \frac{1}{a} A \right) \frac{dr}{d\xi} + \left(\frac{1}{2a} A \mp \frac{2\psi'_c}{Z} \frac{dA}{d\xi} \right) = 0 \quad (53)$$

Equations (50) to (53) are the governing equations which are coupled and should be solved to give Φ (circumferentially average flow coefficient), Ψ (total-to-static pressure rise), A (amplitude of angular disturbances) and r (phase angle of disturbances) as a function of ξ (the non-dimensional time).

The following parameters affect the compressor response during instabilities: the characteristic

steepness (W/H), shut-off head (ψ_{c0}/H), compressor non-dimensional length (l_c), compressor external lag (m), Greitzer parameter (B), throttle characteristic function ($F_T(\Phi)$) and the slope of the compressor axisymmetric characteristic (ψ'_c). One of the advantages of the current model is that it includes the slope of the compressor total to static pressure rise characteristic. The basic Moore-Greitzer equations do not include this parameter. However, if $\psi'_c = 0$ the current model is reduced to the basic Moore-Greitzer model (in that case, Eq. (53) decouples from Eqs. (50-52)). Another advantage of the current model is that it enables the investigation of the stall cell transient behavior, because Eqs. (50) to (53) include $d^2r/d\xi^2$ (stall cell acceleration). Furthermore, $d^2A/d\xi^2$ and $d^2\Phi/d\xi^2$ have appeared in the equations. For reference, the relevant parameters through this paper are: $m = 1.75$, $H = 0.18$, $W = 0.25$, $1/a = 3.5$, $l_c = 8$. Finally, in order to solve the differential equations (Eqs (50) to (53)), Runge-Kutta method is used.

3. VALIDATION

The ability of the modified model developed in the current study in predicting the transient stall cell speed has been approved by comparing the experimental results reported by Jackson (1986) to the theory in Fig. 2, obtained by solving Eq. (52) and (53). The compressor specifications are given in Table 1. The outside lag parameter (m) has been chosen to be equivalent to 2 (see Moore (1984a)). The time lag parameter (a) was then calculated to be equivalent to 0.4889. Finally, the initial conditions imposed are: $d\Phi/d\xi(0) = 0.0$, $A(0) = 0.01$, $dA/d\xi(0) = 0.0$, $dr/d\xi(0) = 0.8$. Note that the choice of $dr/d\xi(0)$ is based on the initial cell speed that Jackson measured (roughly 0.8, as can be observed in Fig. 2). As observed in Fig. 2, the developed model is appeared to predict the transient stall cell speed quite accurately.

Table 1 Jackson (1986) compressor specification

	Rotor	Stator
Solidity	1.43	1.1
Chord (mm)	110	114.6
No. of IGVs	0	
Tip diameter (mm)	1524	
Hub/Tip ratio	0.7	
Speed of Rot. (rpm)	500	

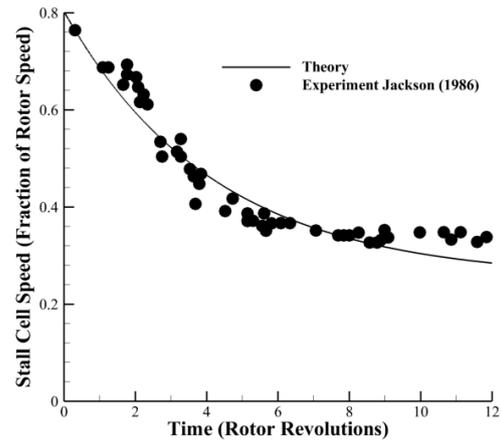


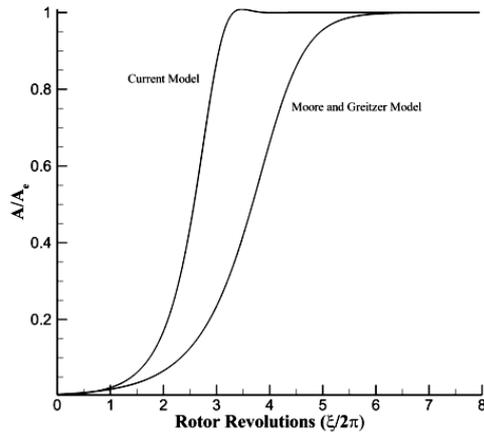
Fig. 2. Transient stall cell speed.

4. RESULT AND DISCUSSION

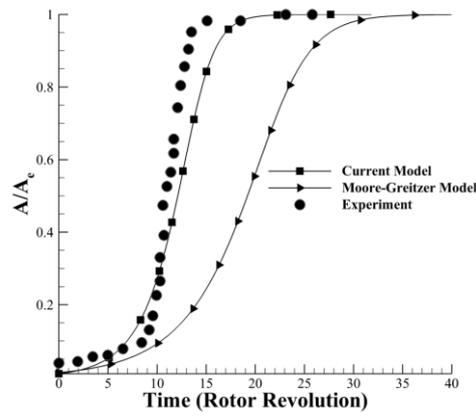
4.1 Pure Rotating Stall

In order to investigate the transient behavior of a stall cell, Eqs. (52) and (53) must be solved together. The mean flow coefficient is chosen to be equivalent to 0.25 ($\Phi = 0.25$), which was also used by Moore and Greitzer (1986). The initial values and the compression system parameters are: $d\Phi/d\xi(0) = 0.0$, $dA/d\xi(0) = 0.0$, $dr/d\xi(0) = 0.6$ and $B = 0.5$, $1/a = 3.5$, $l_c = 8$, $m = 1.75$. A comparison between the stall cell amplitude growth calculated from the current model and that calculated from the basic Moore-Greitzer is given in Fig. 3(a). It should be noted that the initial amplitude of the disturbances is assumed to be $A(0) = 0.01$. Figure 3(a) shows that with the current model, the rate of the amplitude growth is predicted to be steeper and the fully-developed rotating stall pattern to achieve faster, as compared to the basic Moore-Greitzer. The experimental stall cell amplitudes reported by Garnier *et al.* (1991) are adapted and compared to the model in Fig. 3(b). As this figure shows, the current model gives a more accurate prediction of the stall cell amplitudes.

Figures 4(a) and 4(b) show the stall cell amplitude growth and its time derivative for three different values of the initial disturbance amplitudes: $A(0) = 0.1, 0.01$ and 0.001 . Figure 4(a) suggests that the initial disturbance does not have any effect on the final amplitude of the stall cell. However, the greater the initial amplitude, the faster the fully-developed rotating stall is achieved. Furthermore, Fig. 4(b) shows that the rate of the amplitude growth is the same for different initial amplitudes.



a) Comparison between the current model and Moore-Greitzer



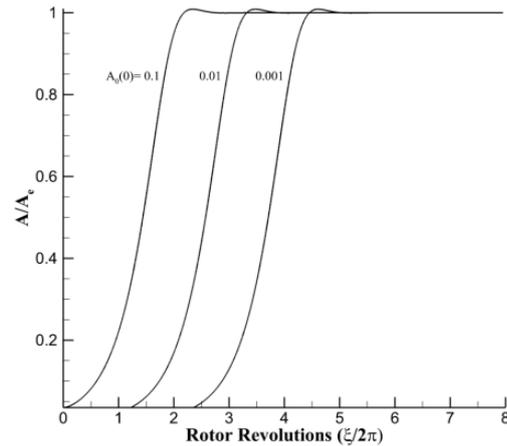
b) Comparison with experiments (Garnier *et al.* (1991))

Fig. 3. Normalized stall cell amplitude.

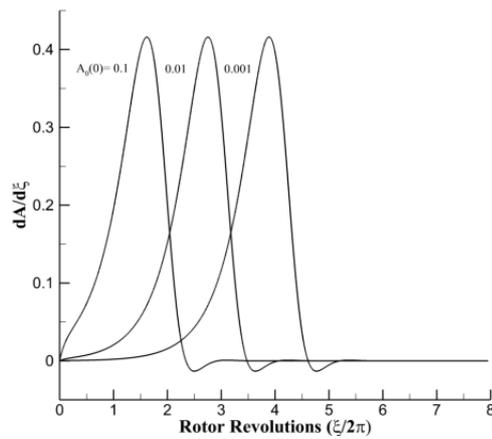
As stated by Koff and Greitzer (1984), the positively sloped portion of the compressor characteristic curve does not have any effect on the steady rotating stall speed. Therefore, the positively sloped part was simply faired in between the peak and valley points (see Fig. 1). In order to investigate the effect of the above mentioned portion of the compressor characteristic on the transient performance of the compressor during rotating stall with the current model, the amplitude growth of the stall cell is shown in Fig. 5 for three different slopes (0.5, 1.08 and 2) at $\Phi = 0.25$, $\Psi = 0.38$. It should be noted that the slope which is specified by Eq. (45) at $\Phi = 0.25$ is equivalent to 1.08. Figure 5 shows that the final amplitude of the stall cell is the same for different initial slopes. However, the transient part is different in that a greater slope causes greater stall cell amplitudes.

4.2 Instability Initiation

In the above section, only Eqs. (52) and (53) were solved together in order to investigate pure rotating stall. Now, by solving the complete governing Eqs. (50-53), the path into instability and the conditions under which the compression system triggers surge or rotating stall can be studied.



a) Normalized stall cell amplitude



b) Growth rate of stall cell amplitude

Fig. 4. Effect of initial disturbance amplitude on the stall amplitude and its rate.

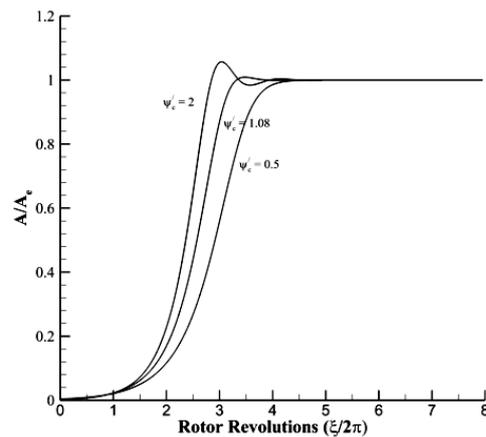
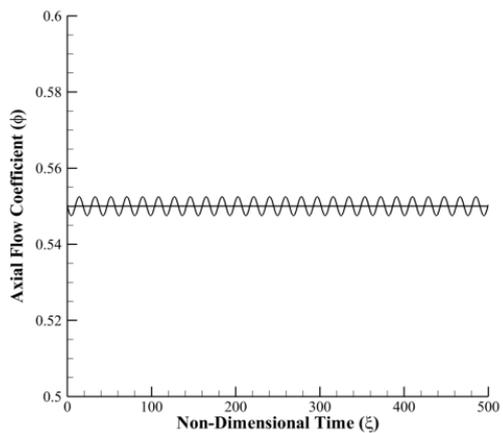


Fig. 5. Effect of the compressor characteristic slope on the stall cell amplitude, $\Phi = 0.25$.

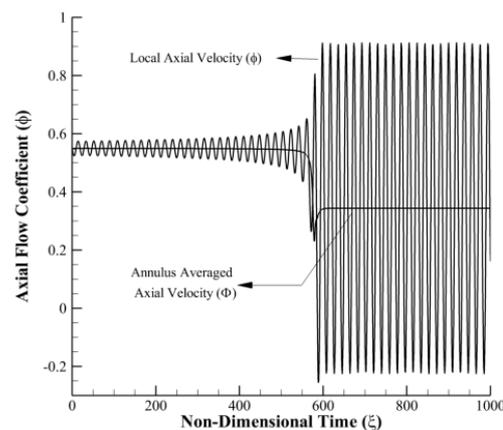
4.2.1 Rotating Stall

As mentioned earlier, Camp and Day (1997) showed that modal rotating stall occurs near the compressor peak pressure rise, $\psi'_c = 0$ (at a slope of the compressor total to static pressure rise characteristic between roughly -0.2 to +0.2). In order to study the effect of initial flow coefficient

on modal stall inception, the governing equations have been solved at $\Phi = 0.55$ (which is in the negative slope portion of the compressor characteristic) for two initial disturbance amplitudes. The initial values and compression system parameters are the same as those used earlier in pure rotating stall. Figure 6(a) and 6(b) show the local and mean flow coefficients for the initial disturbance amplitude equivalent to 0.01 and 0.1, respectively. As Fig. 6(a) shows, the modal disturbances have not neither grown up nor damped, but remained unchanged (note that if the initial disturbance amplitude were smaller enough, this disturbance would damp). If the initial amplitude of the disturbances increases to 0.1 (Fig. 6(b)), the modal waves grow up and cause the mean flow coefficient to suddenly reduce and the local flow coefficient to have large oscillations leading to a fully developed rotating stall pattern. This suggests that with a negative slope of the characteristic, rotating stall can occur if the initial amplitude of the disturbances is large enough, which confirms the results in Camp and Day (1997). Note that in the Moore-Greitzer model, any negative slope causes the modal disturbances to be damped, regardless of the value of the initial disturbances.



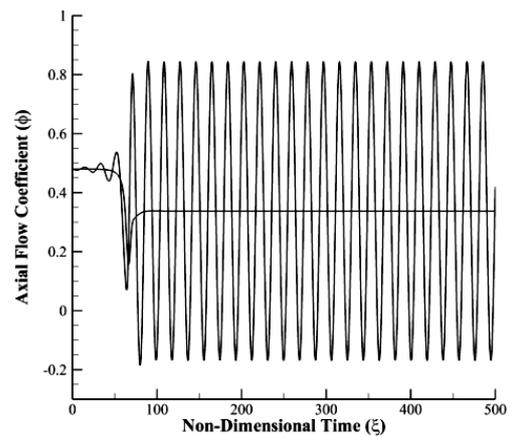
a) $A(0) = 0.01$



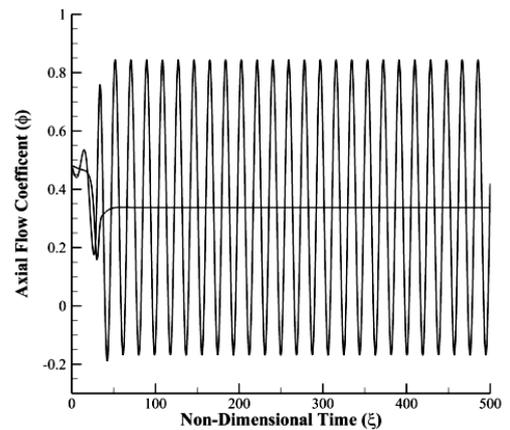
b) $A(0) = 0.1$

Fig. 6. Local and annulus-averaged axial velocity coefficient as a function of time, $\Phi = 0.55$.

Similar to the negative slope, the governing equations have been solved at $\Phi = 0.48$ in the positive slope portion of the characteristic. Figures 7(a) and 7(b) show the local and mean axial flow coefficients for the initial disturbance amplitude equivalent to 0.01 and 0.1, respectively. As seen, rotating stall is triggered in both cases. The two cases are different in that with a greater initial amplitude, the fully developed condition is achieved faster (Fig. 7(b)). Comparing Fig. 7(b) to Fig. 6(b) shows that if the initial operating point is located in the negative slope portion of the compressor characteristic, the time needed for a steady state stall cell formation is much greater than the positive slope.



a) $A(0) = 0.01$



b) $A(0) = 0.1$

Fig. 7. Local and annulus-averaged axial velocity coefficient as a function of time, $\Phi = 0.48$.

4.2.2 Surge

Moore and Greitzer (1986) showed that two parameters (the Greitzer parameter, B , and the compressor mean effective length, l_c) determine the type of the instabilities (surge or rotating stall). In order to investigate surge with the current model, B and l_c have been chosen to be equivalent to 1.2 and 8, respectively, for two initial operating points: $\Phi = 0.48$ and $\Phi = 0.45$. Note further that the initial conditions are:

$d\Phi/d\xi(0) = 0.0$, $dA/d\xi(0) = 0$, $A(0) = 0.01$, $dr/d\xi(0) = 0.0$. Figure 8 illustrates the variation of the mean axial flow coefficient for the two cases modeled. As this figure shows, deep surge is triggered in both cases (the flow coefficient becomes negative). Although the frequency of the instability is the same for the two initial points, surge is deeper for $\Phi = 0.45$.

Figure 9 shows the amplitude of the disturbances as a function of the non-dimensional time. This figure reveals that the disturbances (which identifies the existence of modal waves and rotating stall) first grow up significantly and then become zero (which shows the occurrence of surge). Furthermore, for $\Phi = 0.45$, the growth rate of the disturbances is greater, and therefore, it ends up with surge faster.

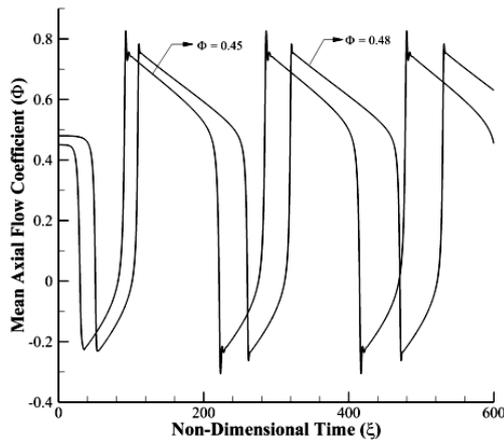


Fig. 8. Annulus-averaged axial velocity coefficient during transient to surge.

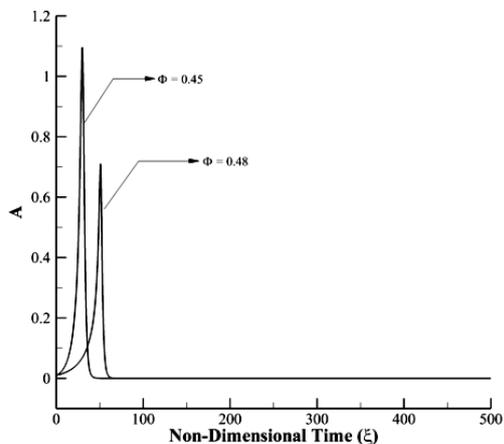


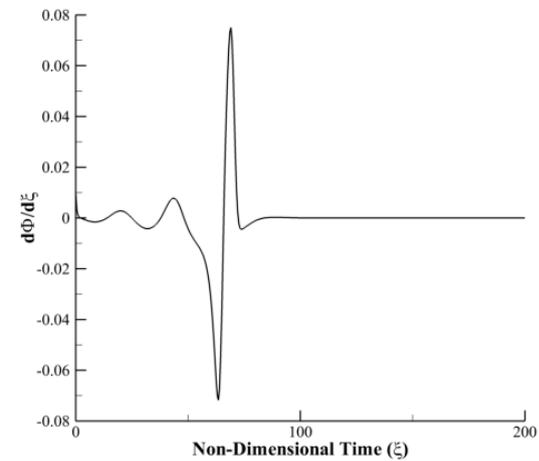
Fig. 9. Disturbance amplitude during transient to surge.

4.2.3 Effect of Throttle Rate

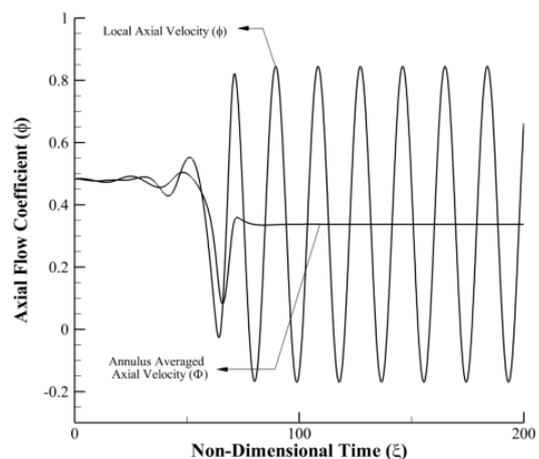
One of the capabilities of the current model is that it enables the investigation of the initial $d\Phi/d\xi$, which can be interpreted as the rate of throttling (it has been experimentally investigated by Garnier *et al.* (1991)). In order to investigate the effect of the throttling rate on the type of the instability, two initial $d\Phi/d\xi$ have been modeled: 0.01 and 0.04. The initial operating

point is at $\Phi = 0.48$, which is located at the positive slope portion of the compressor characteristic. It should be noted that B is chosen to be 0.5, which is less than its critical value (0.8). Therefore, the occurrence of rotating stall is expected. Furthermore, l_c is 8 and the initial values are: $dA/d\xi(0) = 0$, $A(0) = 0.01$, $dr/d\xi(0) = 0.6$.

Figures 10 and 11 show the time variation of the axial flow coefficient and $d\Phi/d\xi$ for the two cases investigated. In Fig. 10, the mean axial flow coefficient has reached a constant value, which identifies the occurrence of fully-developed rotating stall. By increasing the throttling rate to 0.04, however, the annulus averaged flow does not remain constant and shows large oscillations, identifying the occurrence of surge. It can be concluded that the rate of throttling can change the type of the instability in a compression system.



b) $d\Phi/d\xi$



b) Axial flow coefficient

Fig. 10. Local and annulus-averaged axial velocity coefficient as a function of time (initial $d\Phi/d\xi = 0.01$).

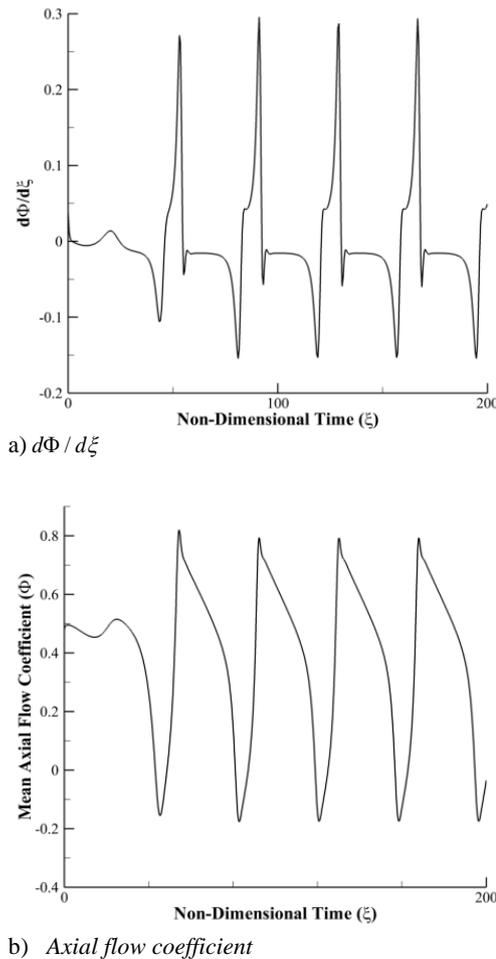


Fig. 11. Local and annulus-averaged axial velocity coefficient as a function of time (initial $d\Phi/d\xi = 0.04$).

5. CONCLUSION

A new model has been developed by modifying the basic Moore-Greitzer theory. The general assumptions were similar to those of the Moore-Greitzer model. However, a second order hysteresis was assumed for the pressure rise of the rotor and stator rows, which added new parameters to the governing equations. The modified model has some advantages and new capabilities, as compared to the basic Moore-Greitzer. One of these advantages is that the governing equations in the current model include the slope of the compressor characteristic curve. It was shown that in the positive slope portion of the compressor characteristic, ψ'_c does not affect the final stall cell speed and its amplitude. However, the transient stall cell behavior was shown to be different having different slopes. Results further revealed that ψ'_c changes the fully-developed rotating stall characteristic. The effect of the initial amplitude of the disturbance on the stall cell behavior was also investigated in the current study and it was shown that it does not change the stall cell final speed and amplitude. It was shown in the current study that if the initial operating point is located in the negative slope part of the compressor

characteristic, the disturbances may be damped, kept unchanged or grown up to fully-developed rotating stall, depending on their initial amplitudes. If the initial point is located in the positive slope part, however, the disturbances were shown to be grown up to rotating stall, regardless of their initial amplitudes. Another finding was that in the positive slope portion, the fully-developed rotating stall is achieved considerably faster, as compared to the negative slope. An advantage of the current model is that it includes the second derivative of the mean axial flow coefficient ($d^2\Phi/d\xi^2$). This enables the investigation of the initial $d\Phi/d\xi$, which can be interpreted as the rate of throttling. It was shown that the rate of throttling can change the type of instability (e.g., rotating stall to surge).

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